

## Cryogenic Research for HTS Transmission Cables in Korea

- Overview 10 min
- 10 kW Brayton Refrigerator 10 min
- He-LN<sub>2</sub> Heat Exchanger 15 min
- Cryogenic Design for Future 15 min

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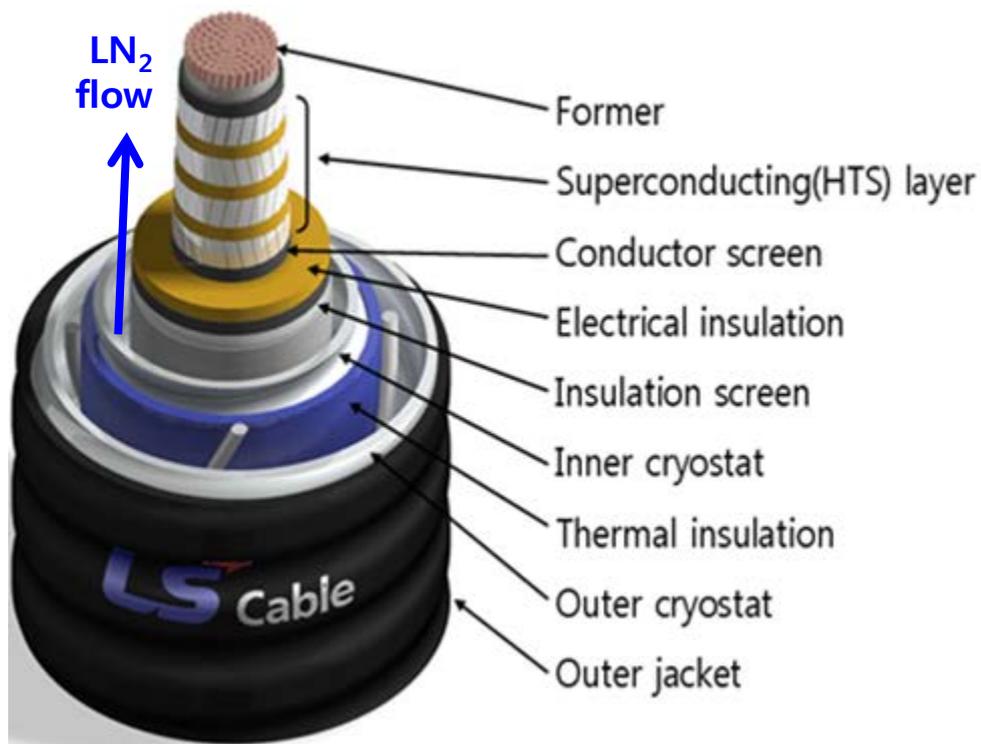
## ➤ Why Superconducting (HTS) Cables?

- Efficiency      Less transmission loss
- Environment    Less CO<sub>2</sub> emission
- Power density    More energy per unit area

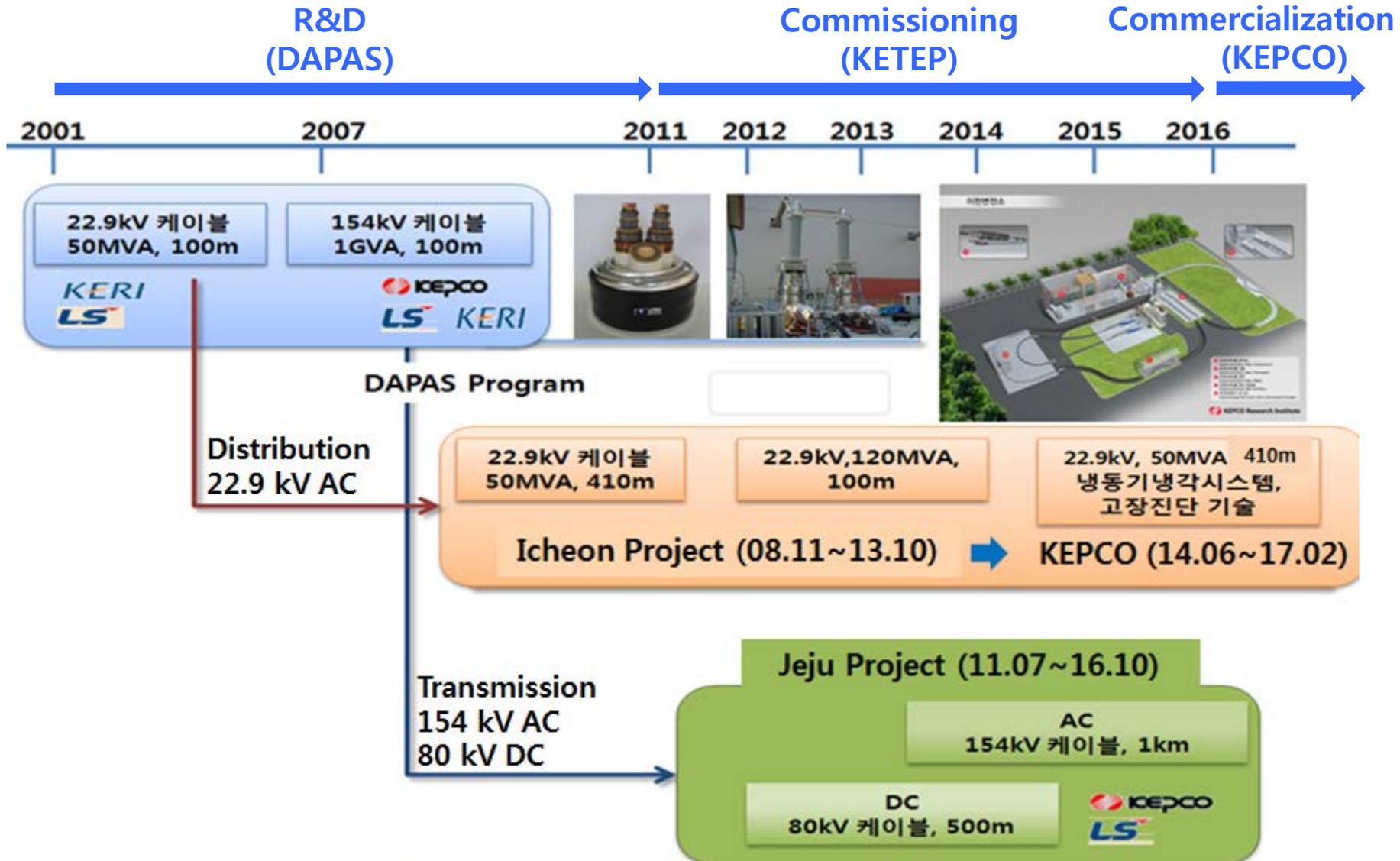
(Cryogenic Cooling?)

(Cryogenic Cooling?)

(Yes)



## 15 Years of HTS Transmission Cables in KOREA



## ➤ Jeju Project (154 kV AC, 1 km) – Completed in March 2016

- Transmission Grid in Juju Island
- 3 Phase in 3 Cryostats (2 Go's + 1 Return)
- Started 6 month-operation (March-Sept, 2016)



Brayton Refrigerator (7 kW)



Terminals



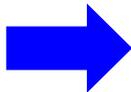
Stirling Coolers (3 kW x 2)



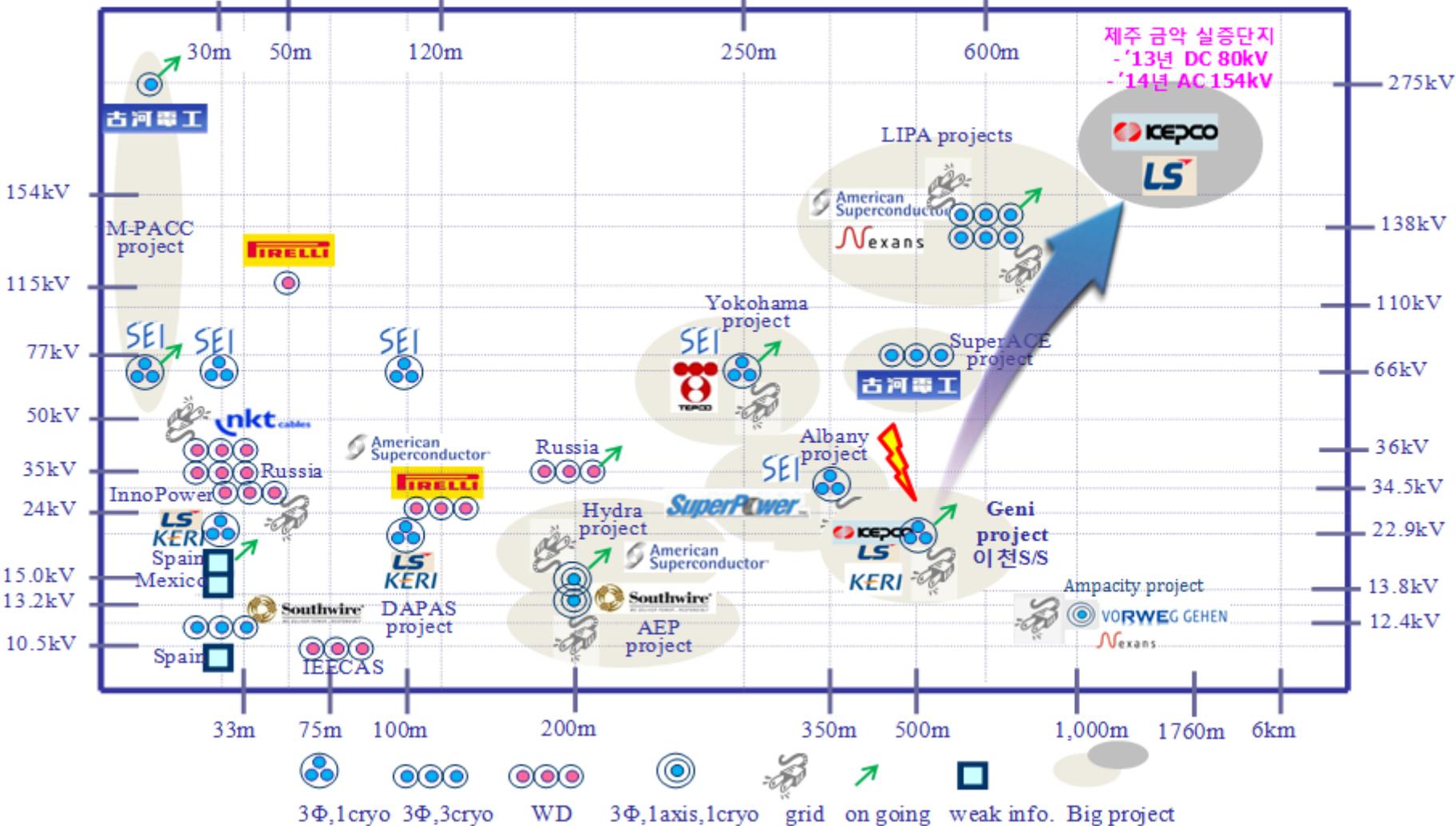
LN<sub>2</sub> Circulation System

➤ A World Record in HTS Cable

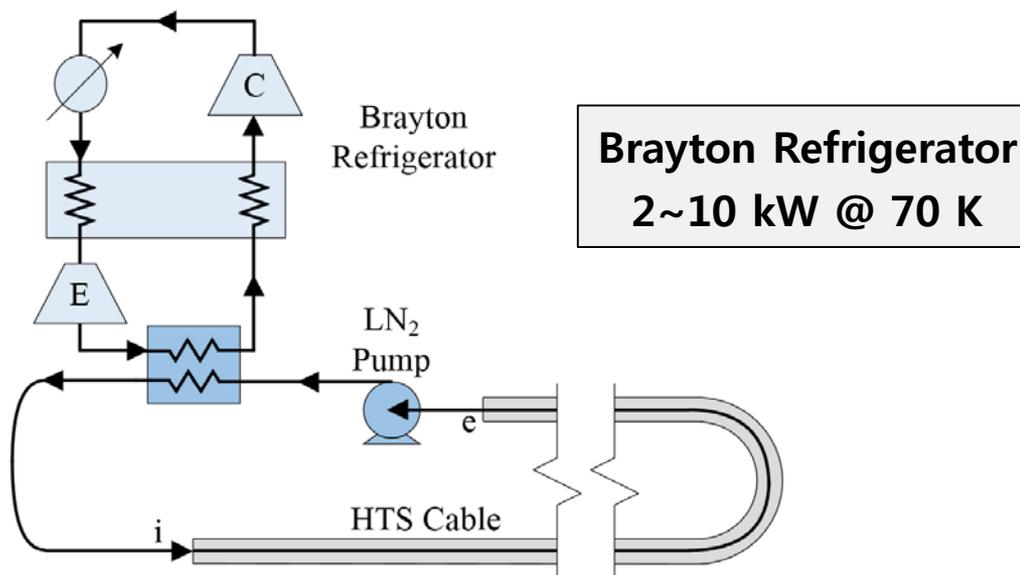
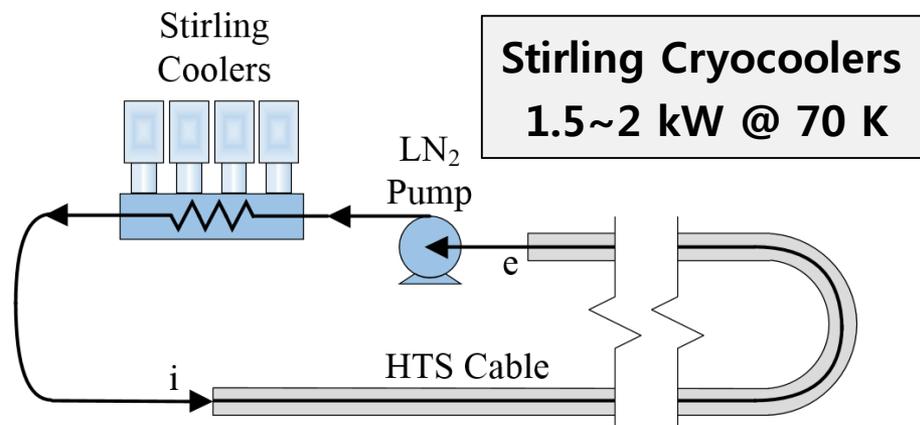
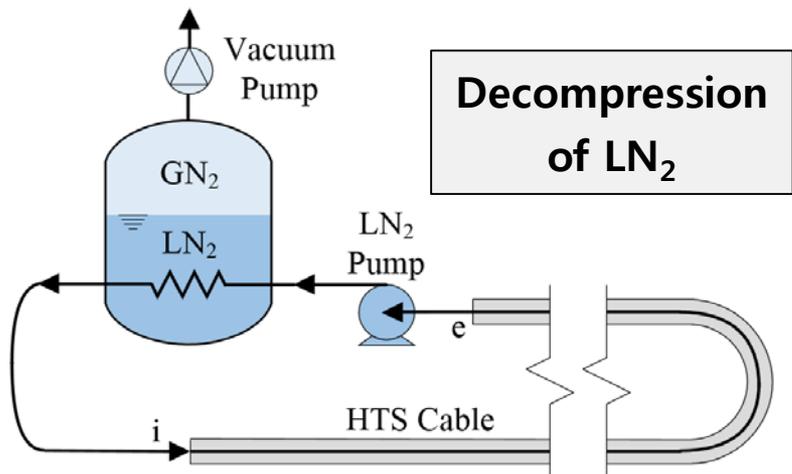
**LIPA**  
(AMSC+Nexans)  
138 kV 610 m



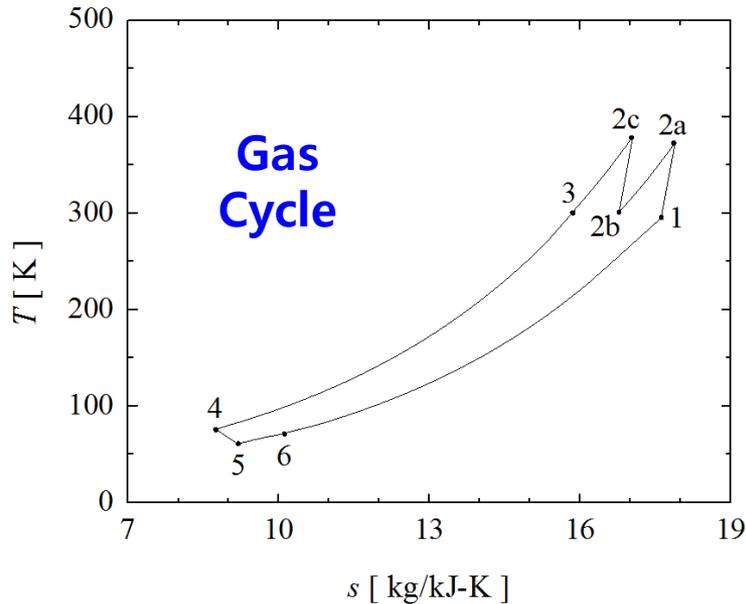
**Jeju**  
(KEPCO+LS)  
154 kV 1 km



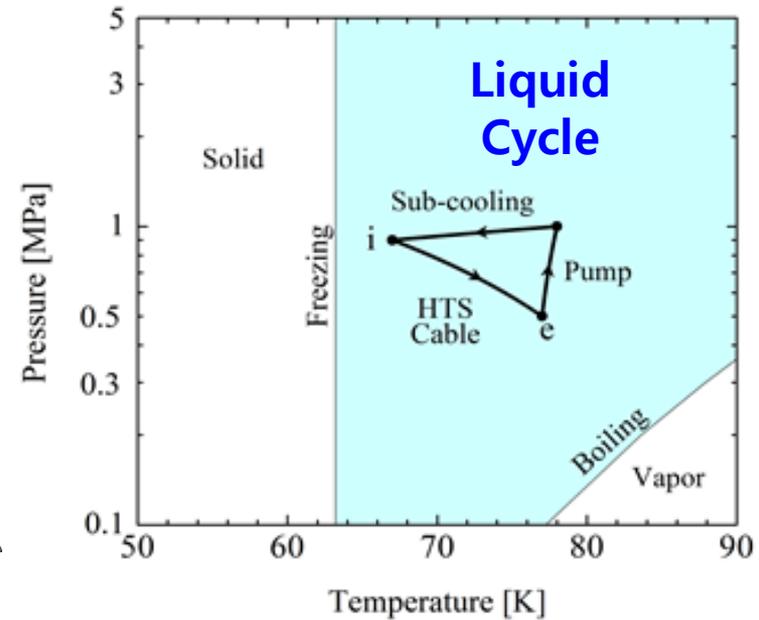
## ➤ Cryogenic Refrigeration of HTS Cables



## ➤ Refrigeration Cycle (He or Ne)

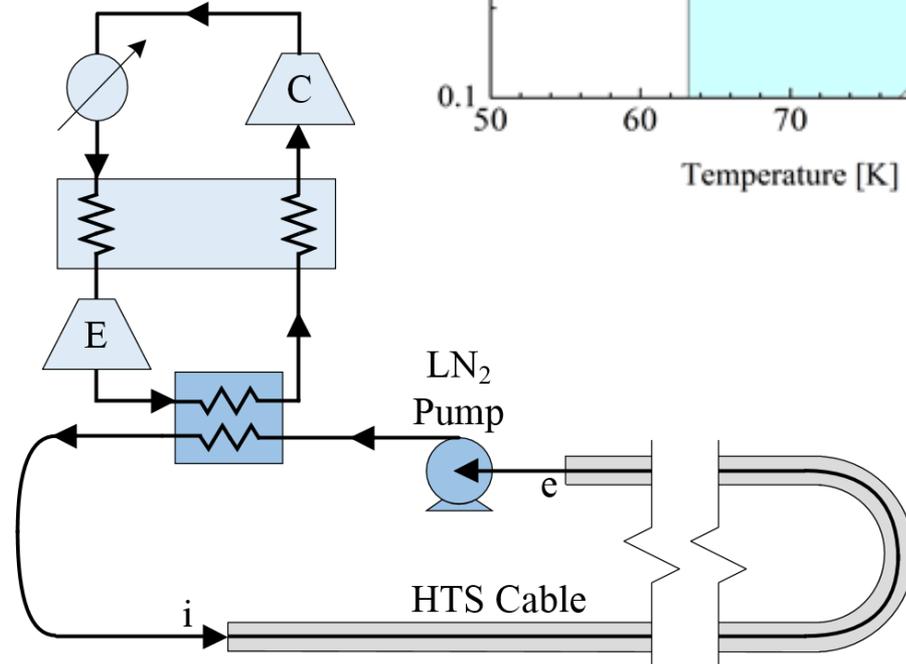


## ➤ Coolant Cycle (LN<sub>2</sub>)



## ➤ Three Key Issues

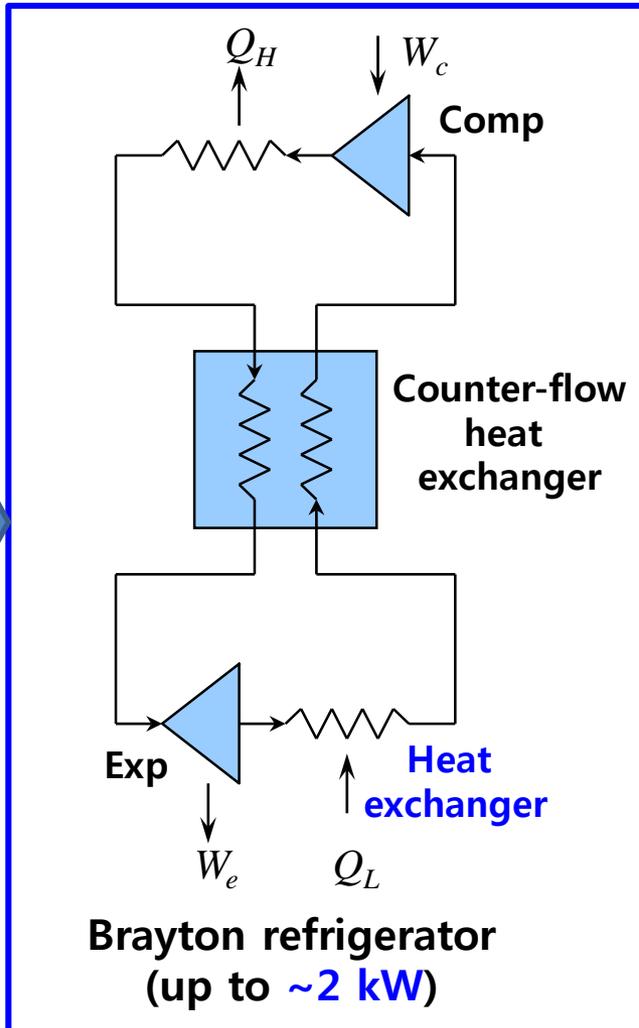
- Refrigerators
- Heat Exchangers
- LN<sub>2</sub> Circulation



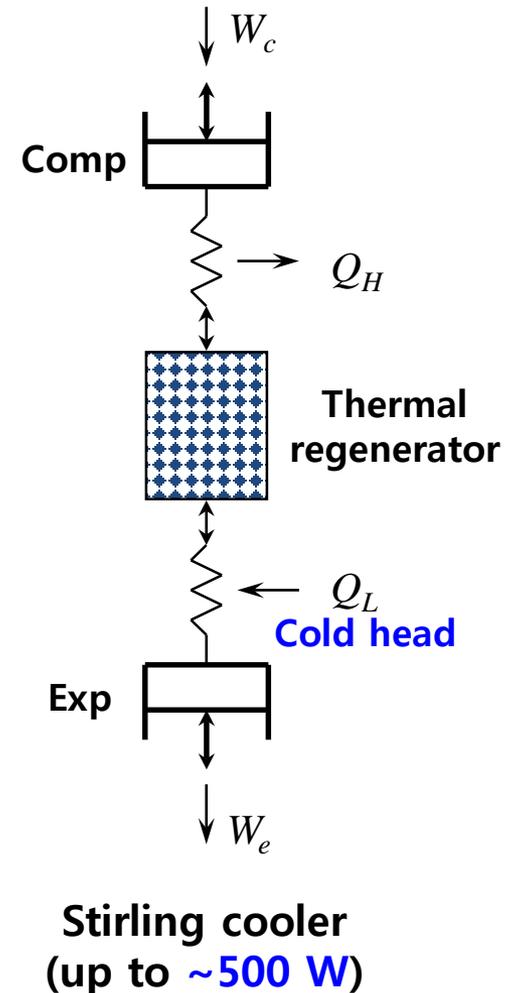
- Overview
- **10 kW Brayton Refrigerator**
- He-LN<sub>2</sub> Heat Exchanger
- Cryogenic Design for Future

➤ Cryogenic Refrigeration at 60-70 K

## Recuperative Cycle



## Regenerative Cycle



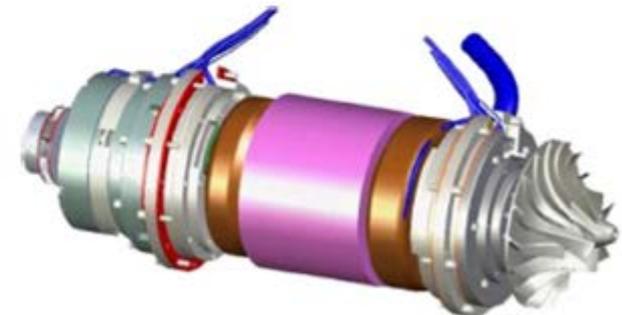
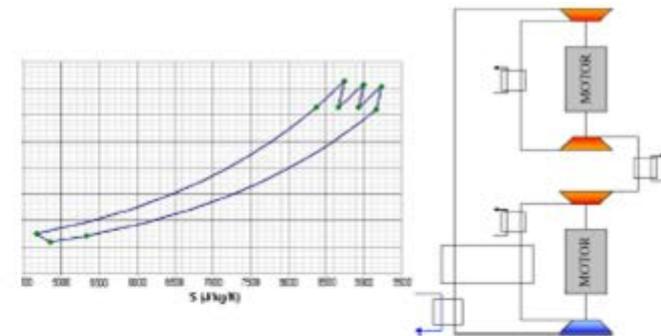
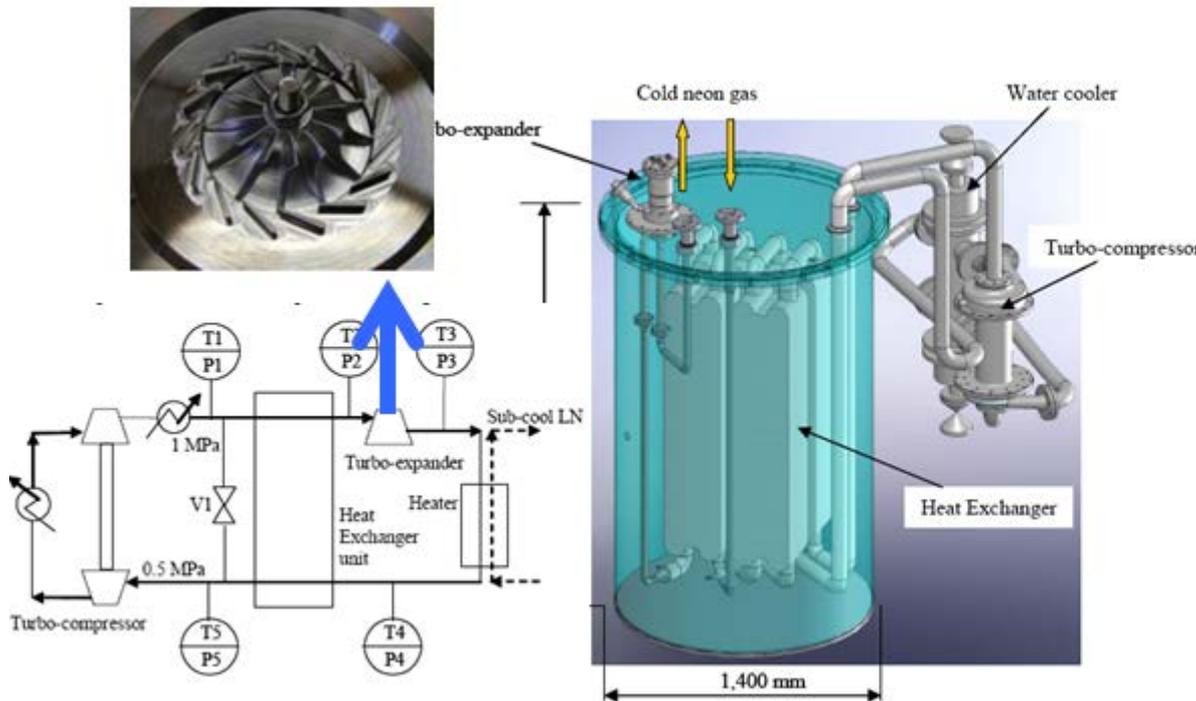
## ➤ Brayton Refrigerators (State-of-the-Art 2011)

### (1) Taiyo Nippon Sanso (CEC 2011)

- Refrigerant Ne
- Capacity 2 kW
- FOM (%Carnot) ~ 17% (measured)
- Ready for delivery

### (2) Air Liquide (IEEE TAS 2011)

- Refrigerant He
- Capacity 11~22 kW
- FOM (%Carnot) ~ 24% (?)
- Under development (over \$6M)





## ➤ Thermodynamic Structure

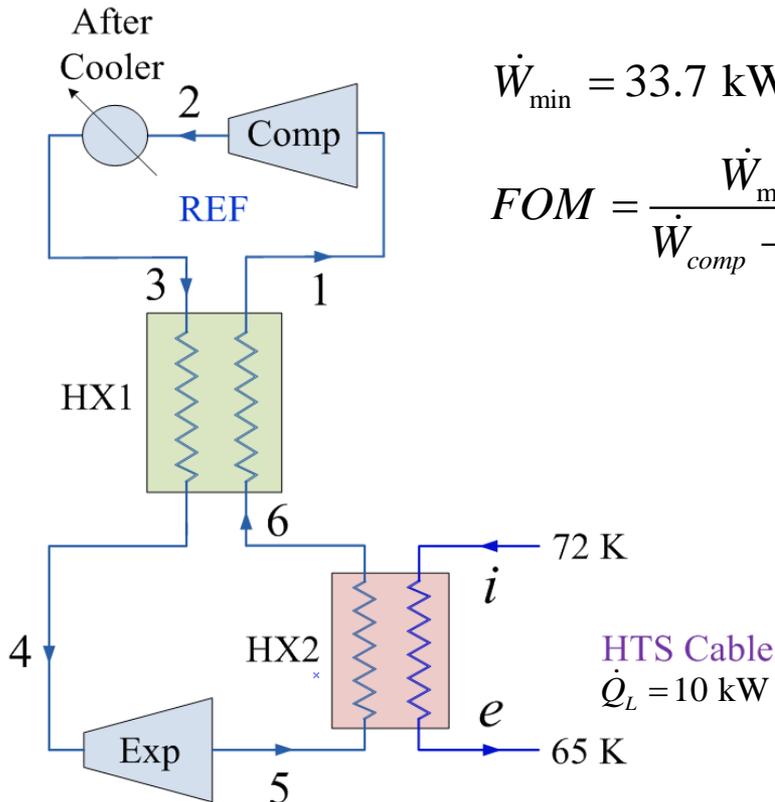
	Standard	2-Stage Expansion	Dual Turbines
Low-Pressure Cooling			
High-Pressure Cooling			

## ➤ Modeling and Design Basis

$$\dot{m}_{LN} = \frac{\dot{Q}_L}{h_i - h_e} = 0.71 \text{ kg/s}$$

$$\dot{W}_{\min} = 33.7 \text{ kW}$$

$$FOM = \frac{\dot{W}_{\min}}{\dot{W}_{\text{comp}} - \dot{W}_{\text{exp}}}$$



Adiabatic Efficiency	Comp	75%
	Exp	75%
Minimum Temperature Difference	HX1	5 K
	HX2	1.5 K
Pressure Drop	HX1	50 kPa
	HX2	20 kPa
	AC	20 kPa



Aspen HYSYS®

V7.1

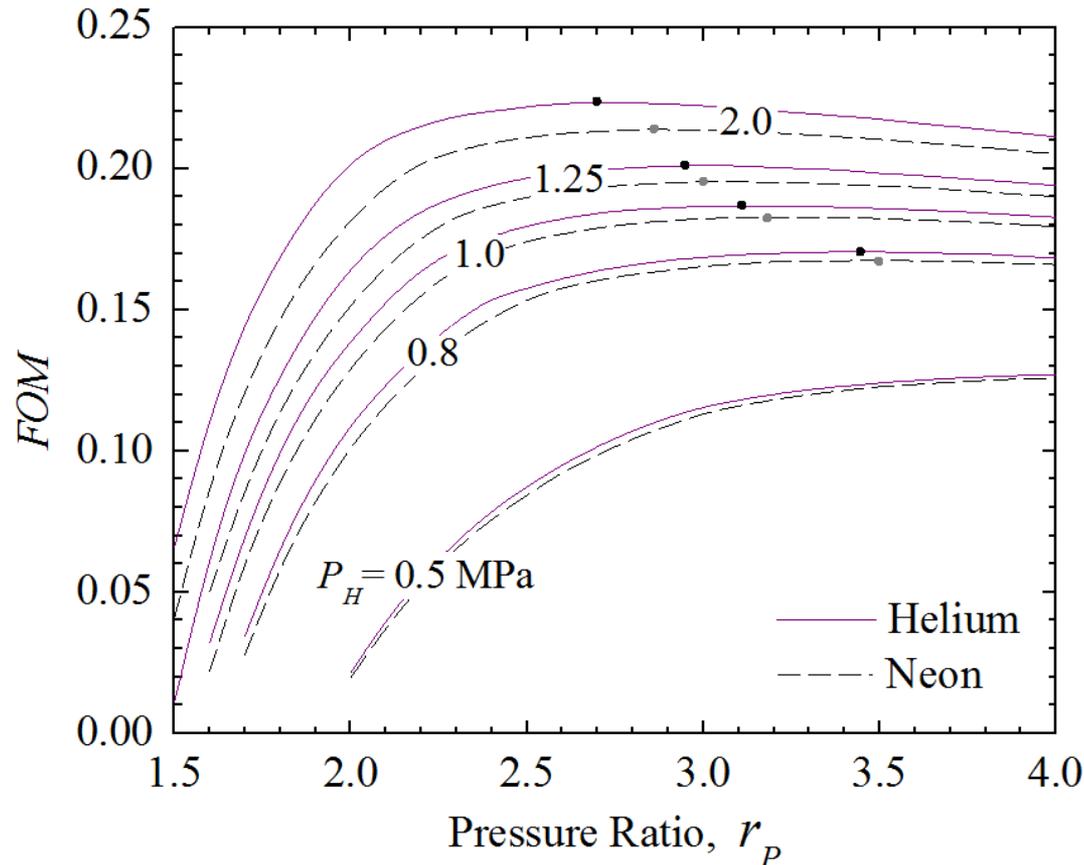


aspen ONE™

➤ Properties of He and Ne

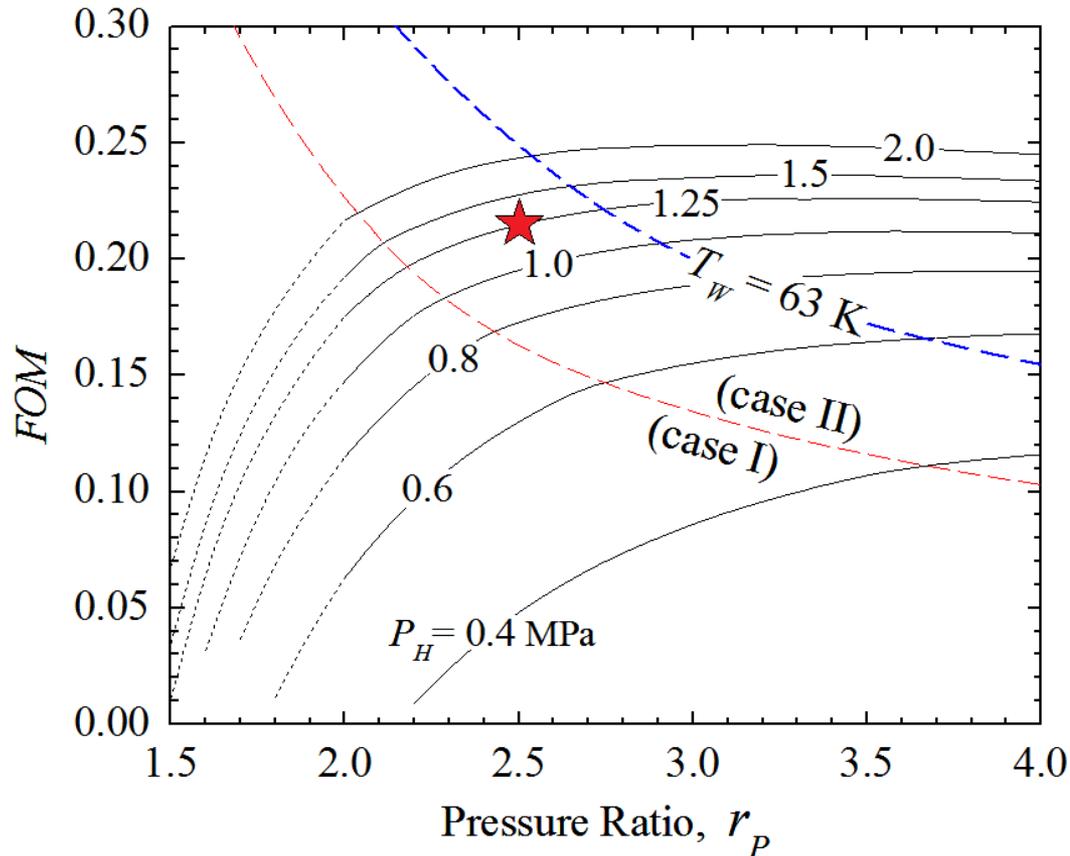
	Helium (He)			Neon (Ne)		
Specific Heat Ratio	1.667			1.667		
Molecular Weight [kg/kmol]	4			20.18		
	65K	200K	300K	65K	300K	200K
Thermal Conductivity [W/m K]	0.045	0.0926	0.1203	0.016	0.0489	0.0374
Viscosity [ $10^{-5}$ Pa-s]	0.62	1.52	2.11	1.07	3.5	2.51
Density [ $\text{kg/m}^3$ ]	0.751	0.244	0.163	3.802	0.819	1.229

## ➤ Selection of Refrigerant (He or Ne)



- ✓ Nearly same FOM at low pressures
- ✓ He is superior to Ne as pressure increases over 1 MPa
- ✓ Select He and operate at  $P > 1.25$  MPa

## ➤ Operating Pressure (He)

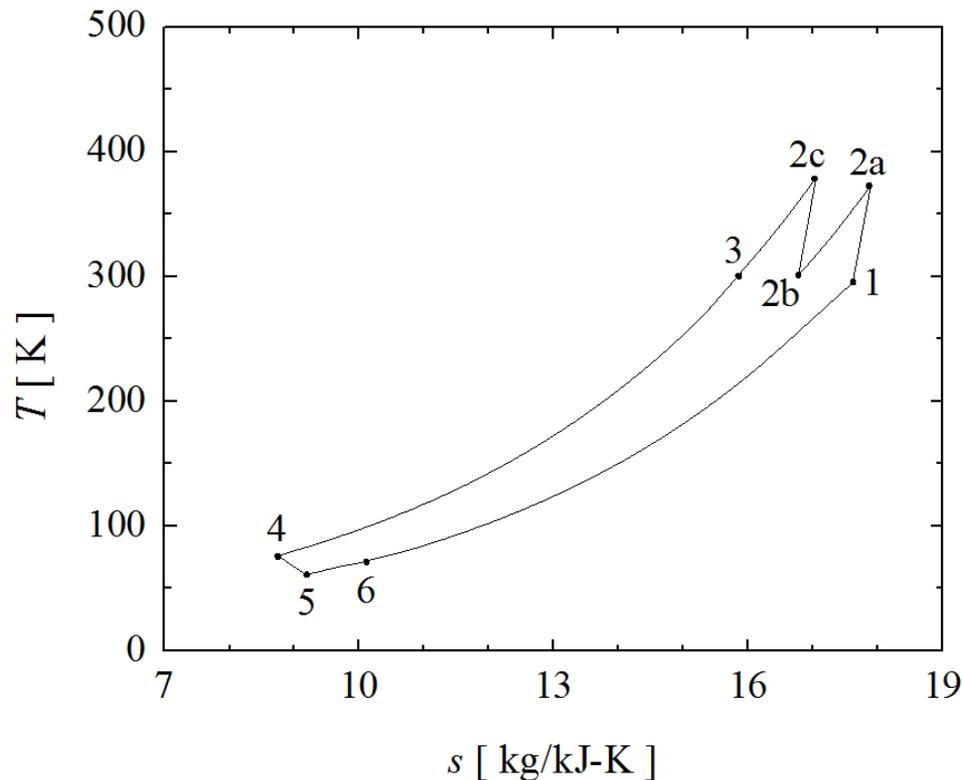


- ✓ There exist an **optimal pressure** ratio to maximize FOM.
- ✓ Temperature may drop below the **freezing temperature** of LN<sub>2</sub> at high P's.
- ✓ Design Condition ★  $P_H = 1.25 \text{ MPa}$ ,  $P_L = 0.5 \text{ MPa}$  ( $r_p = 2.5$ )

## ➤ Results: Designed Cycle

P ratio	FOM	Ref	Wall T (HX2)	$P_{max}$	Mass Flow	$W_{in}$	Comp
2.5	21.4%	He	> 64 K	1.25 MPa	0.209 kg/s	158 kW	2-Stage

## ➤ T-s Diagram and Properties



### Refrigerant: Helium

	$P$ (MPa)	$T$ (K)	$h$ (J/g)	$s$ (J/g-K)
1	0.506	295.0	-16.86	17.61
2a	0.801	374.0	393.9	17.89
2b	0.791	300.0	9.07	16.77
2c	1.25	380.4	426.9	17.06
3	1.24	300.0	8.78	15.84
4	1.19	75.80	-1159.5	8.750
5	0.576	61.38	-1232.9	9.165
6	0.556	70.50	-1185.1	9.964

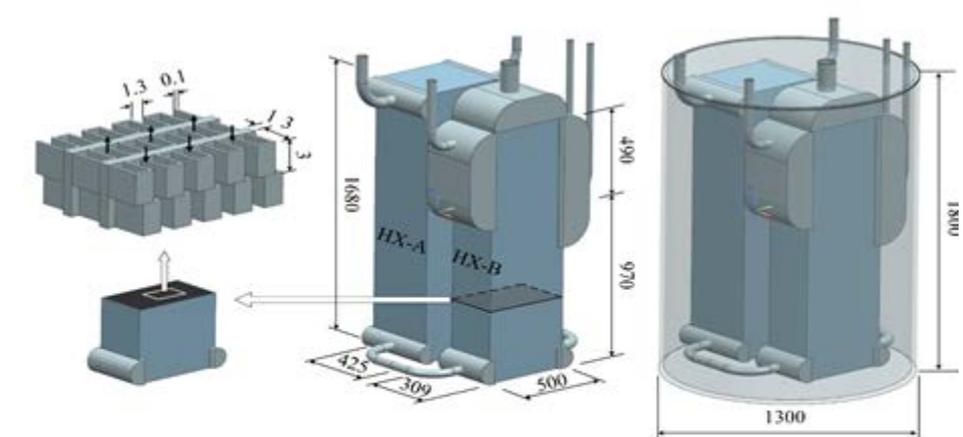
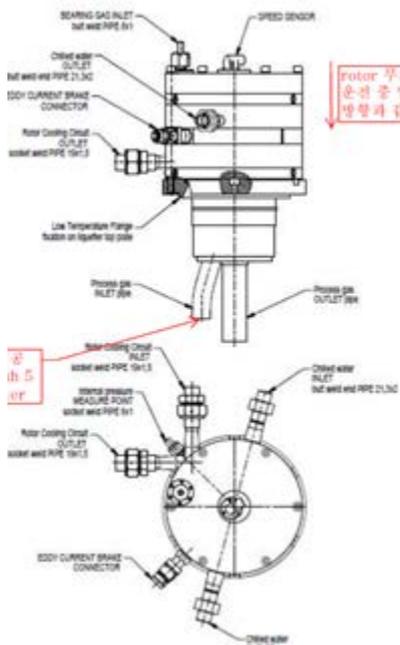
## ➤ Fabrication and Construction (Plan to Test in May 2016)

### • Turbo-Expanders (ATEKO, CZECH)

Flow direction: Radial Flow-in  
 Bearing: He Gas bearing  
 Output power: Eddy Current Brake  
 Rotor diameter: 30.5 mm  
 Rotor velocity: 180,000 rpm  
 Pressure ratio: 2.07

### • Plate-Fin Heat Exchangers (DongHwa, KOREA)

	HX-A	HX-B	
<b>Material</b>	Aluminum 3003		
<b>Number of layers</b>	39 (Warm) 65 (Cold)	35 (Warm) 45 (Cold)	
<b>Height</b>	425 mm	309 mm	309 mm
<b>Length</b>	1680 mm	970 mm	446 mm
<b>Width</b>	500 mm	500 mm	500 mm

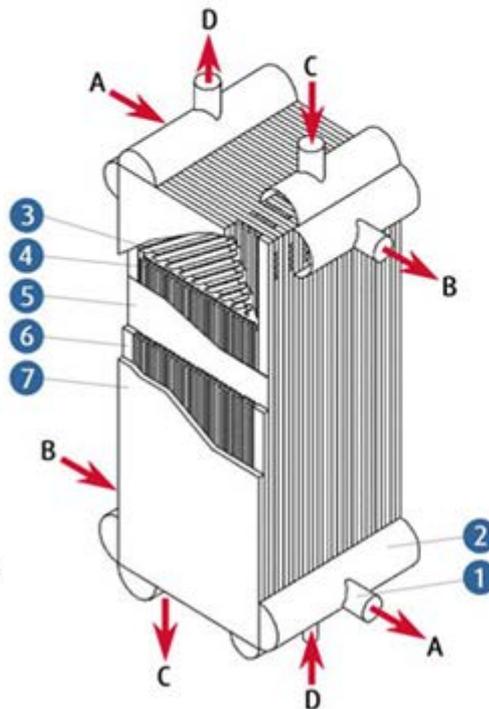
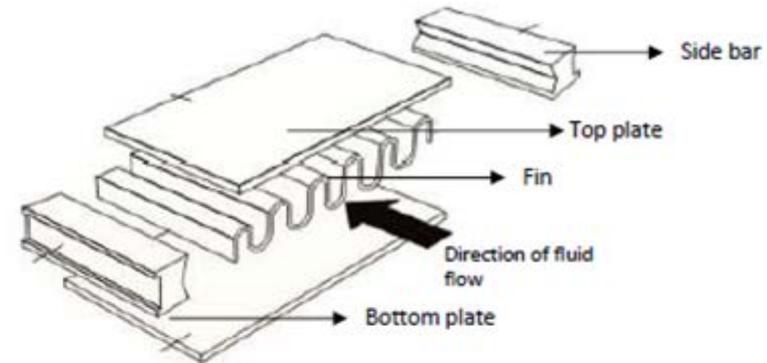


- Overview
- 10 kW Brayton Refrigerator
- **He-LN<sub>2</sub> Heat Exchanger**
- Cryogenic Design for Future

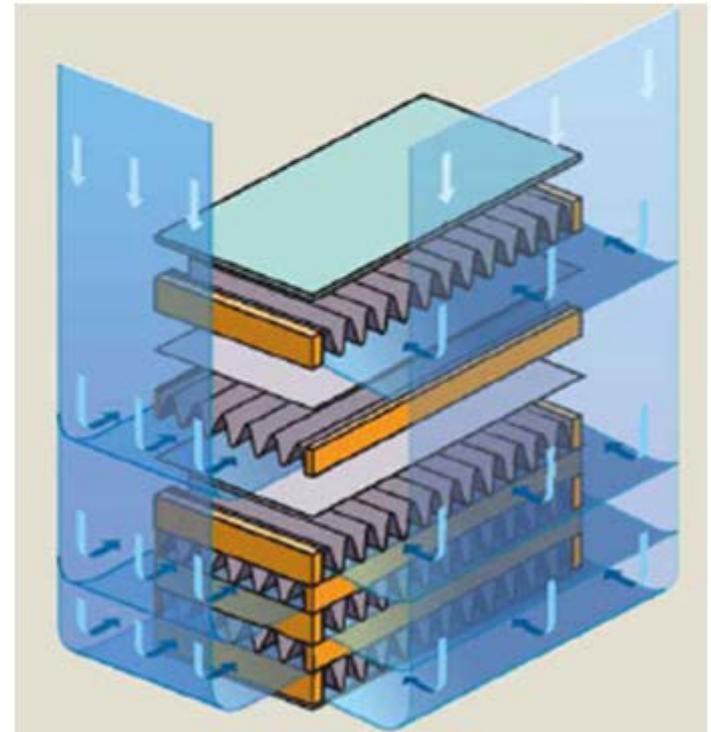
## ➤ Plate-Fin Heat Exchangers (PFHX)

- Widely Used in Cryogenic Systems
- Brazed **aluminum** fins and plates
- Compactness (Large **surface area** / volume)
- Design **flexibility**

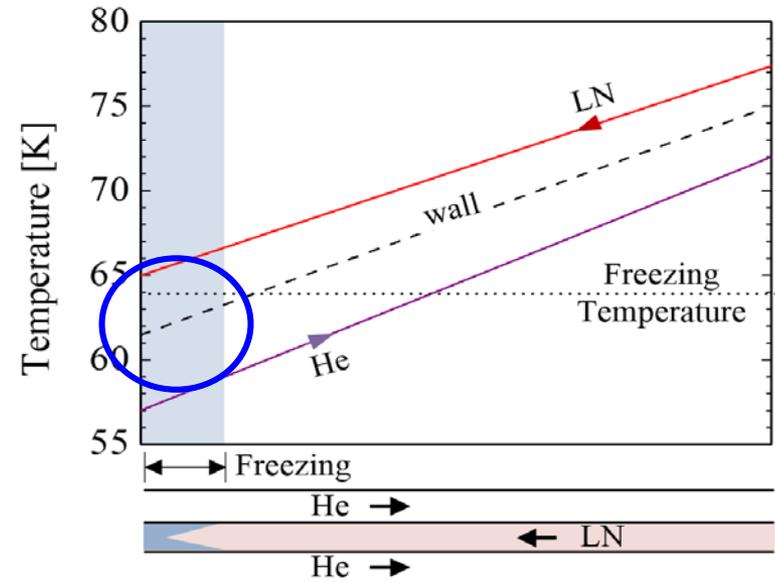
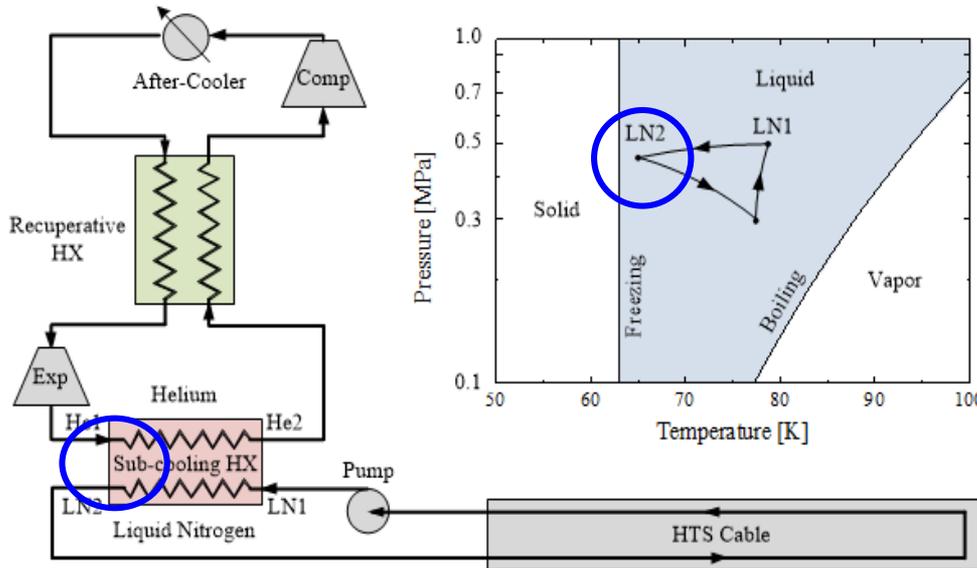
⇒ Counter-flows, Cross-flows, Multi-streams etc.



- 1 Stub pipe
- 2 Header tank
- 3 Distributor fin
- 4 Heat transfer fin
- 5 Partition plate
- 6 Side bar
- 7 Cover plate



## ➤ Important Design Issue – Possibility of LN<sub>2</sub> Freeze-out



✓ Need for **Long-Length** HTS Cables (1~3 km)

→ Required Cold LN<sub>2</sub> Supply near **Freezing Temperature (63.4 K)**

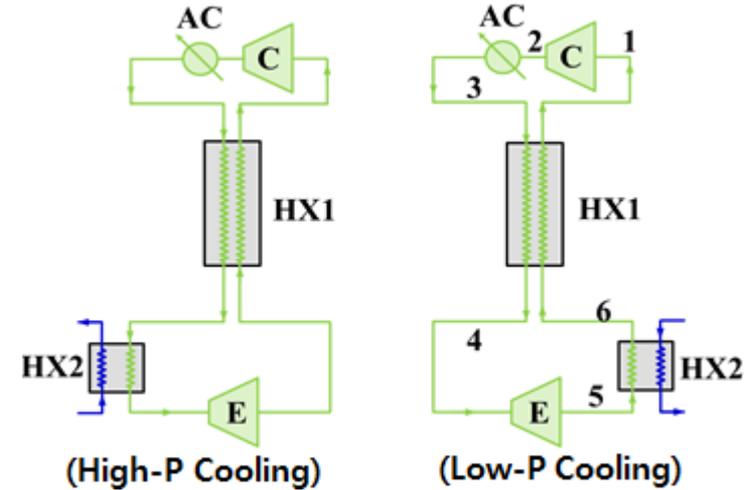
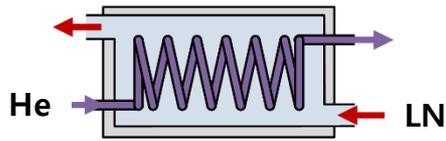
✓ Practical **Fluctuation** of Thermal Load and/or Operating Condition

✓ Stoppage of LN<sub>2</sub> Flow due to Freeze-out

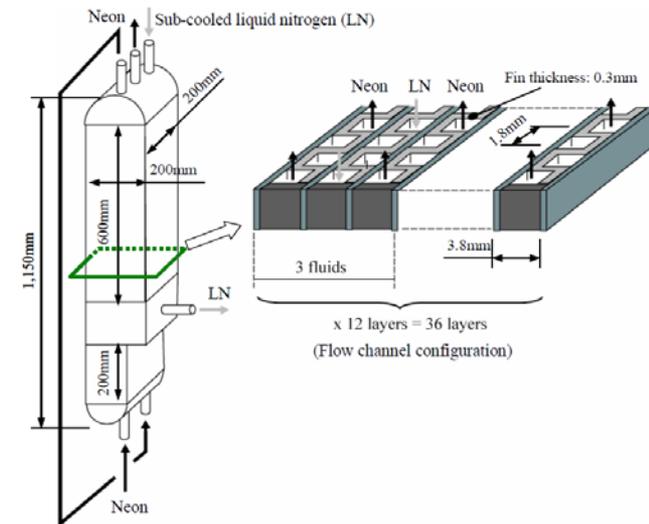
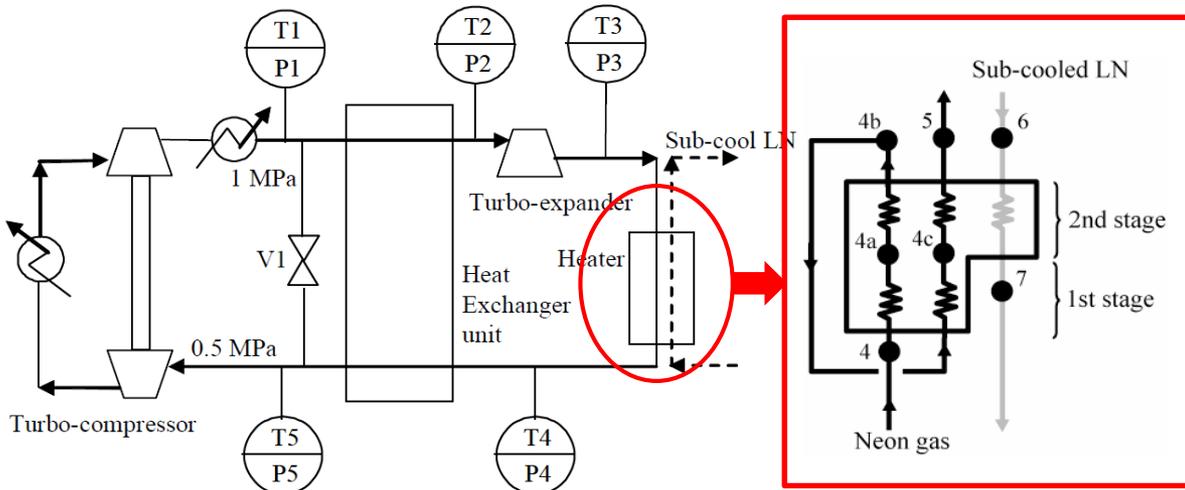
→ Hazard of **Disastrous Accident** followed by a Loss of HTS Cooling

## ➤ Existing Anti-Freezing Schemes (Taiyo Nippon Sanso, CEC, 2012)

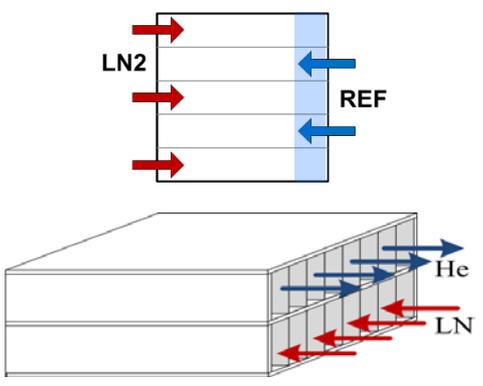
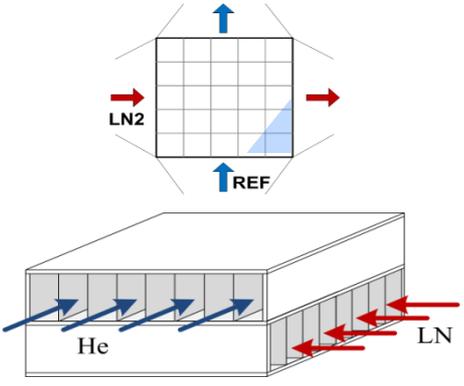
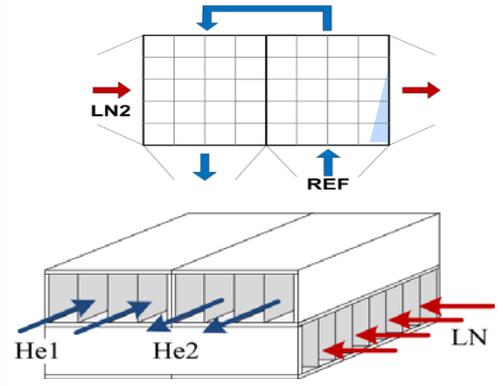
- Refrigeration Cycle with **High-Pressure Cooling**  
⇒ Penalty in thermodynamic efficiency
- **Tube-in-Bath** HX ⇒ Low effectiveness



- **Two-stage HX** ⇒ Penalty of large  $\Delta P$

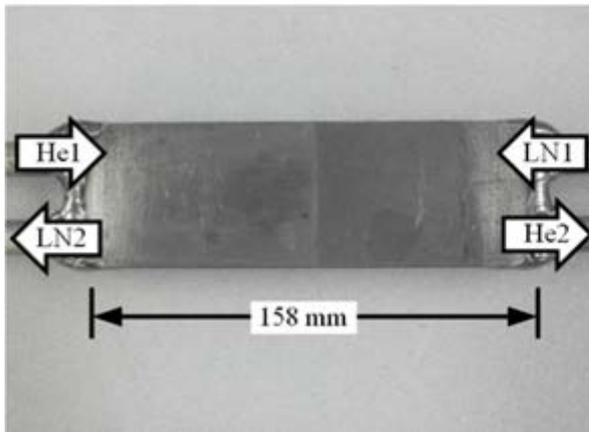


➤ New Proposal of Anti-Freezing Scheme (Chang et al., Cryogenics, 2013)

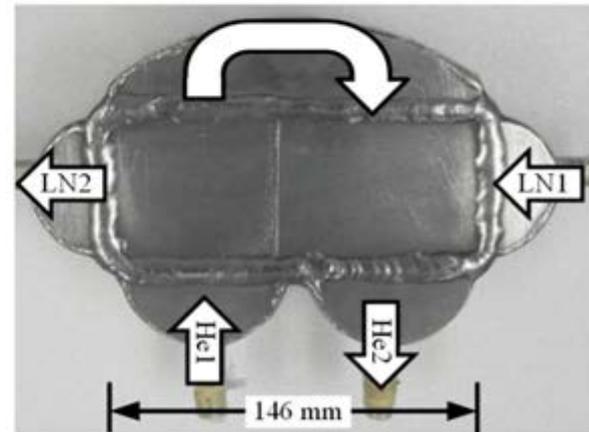
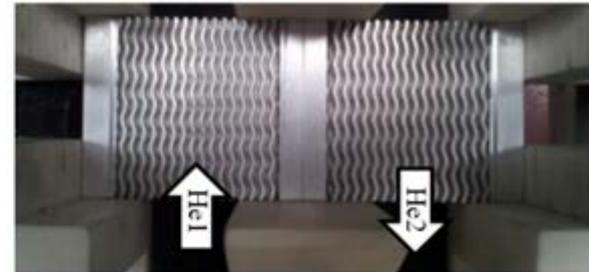
	Counter-Flow	Cross-Flow	2-Pass Cross-Flow
Structure			
Temperature Distribution	1-Dimensional	2-Dimensional	2-Dimensional
Freeze-out Safety	Poor	Good	Good
Heat Exchange Effectiveness	Good	Poor	Fair

## ➤ Fabrication of PFHX's for Experiment

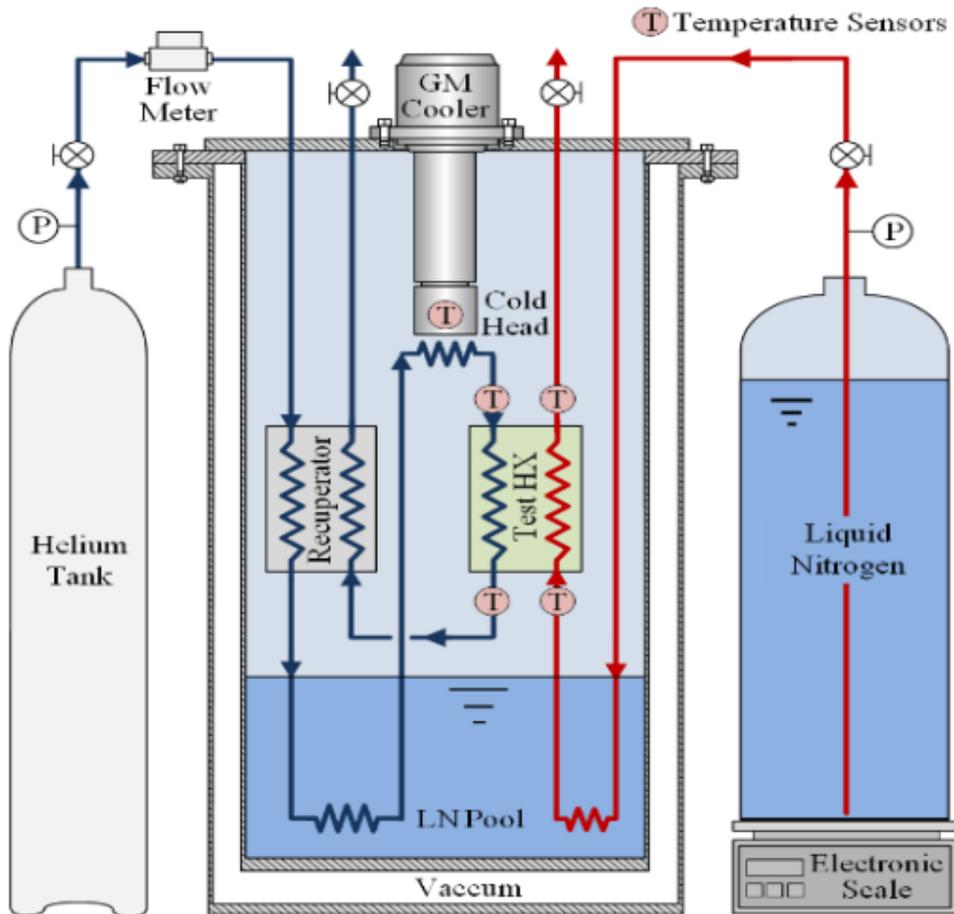
### Counter-Flow HX



### 2-Pass Cross-Flow HX

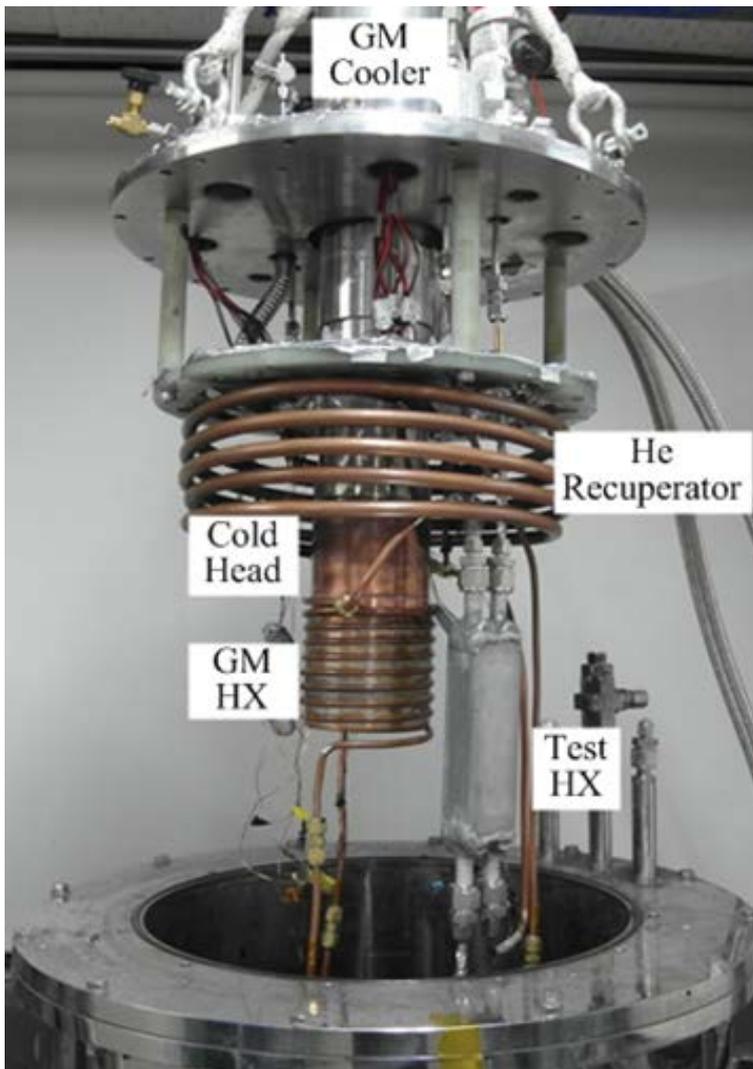


➤ Experimental Set-up (Chang et al., Cryogenics, 2013)

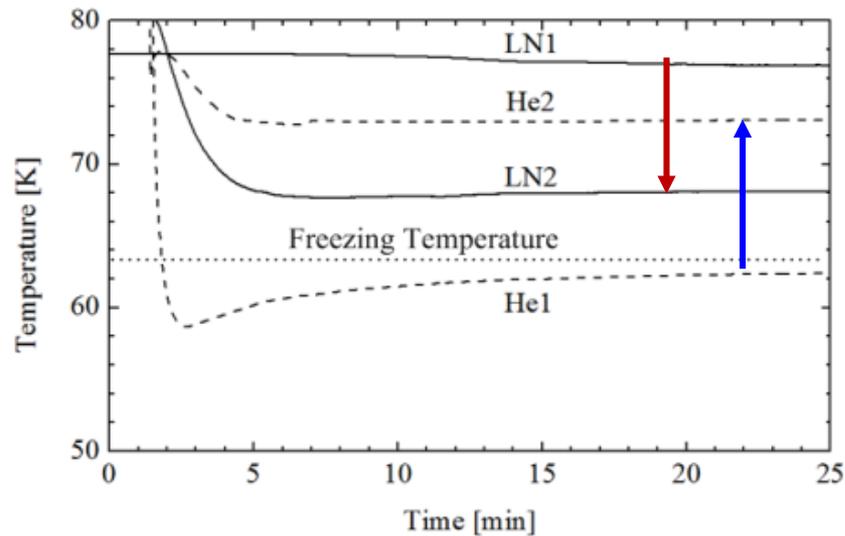


- Counter-Flow vs. 2-Pass Cross-Flow
- Gas He
  - LN Pool and GM Cooler (SHI 500B)
  - Temperature Control by a Heater
  - Generation of Freezing Condition
- Liquid N<sub>2</sub>
  - Compressed Liquid at ~ 0.4 MPa
  - Constant Inlet Temperature (77.5 K)
- Silicon Diode T Sensors
- He Flowmeter
- Electronic Scale for LN<sub>2</sub> flow rate

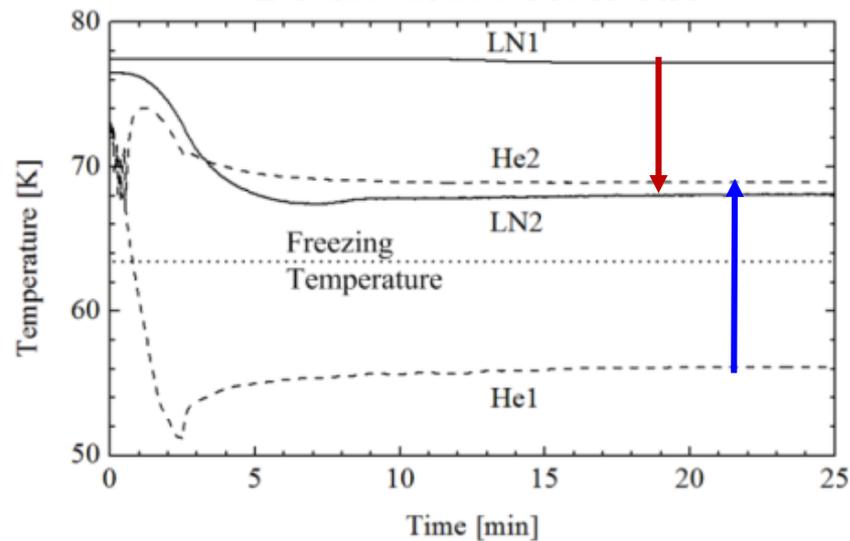
## ➤ Apparatus and Procedure



### Counter-Flow HX

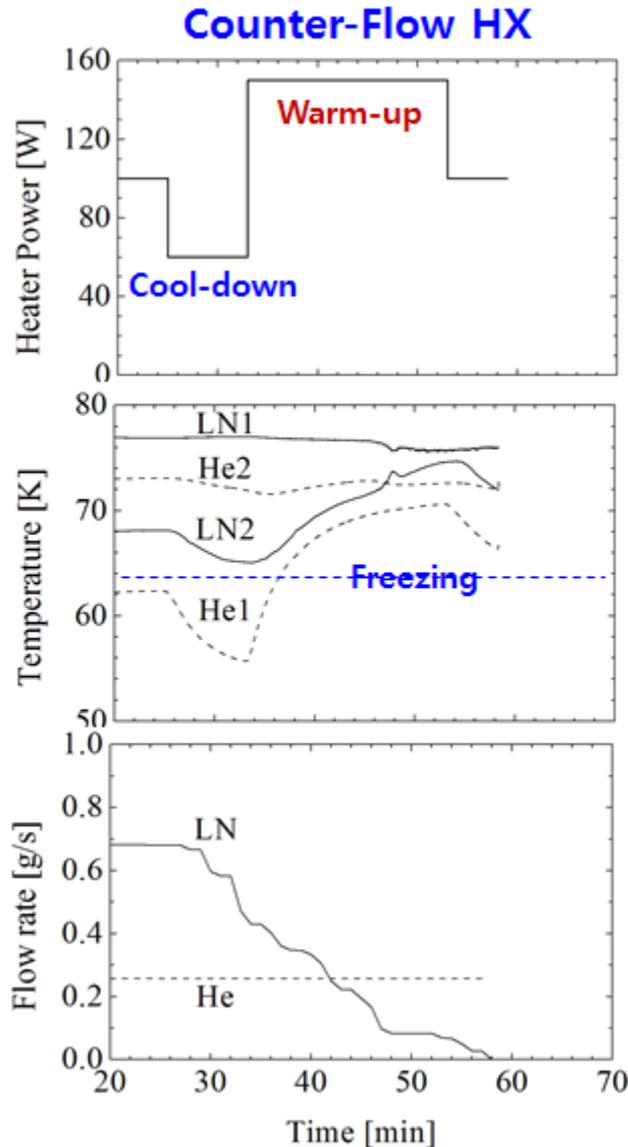


### 2-Pass Cross-Flow HX

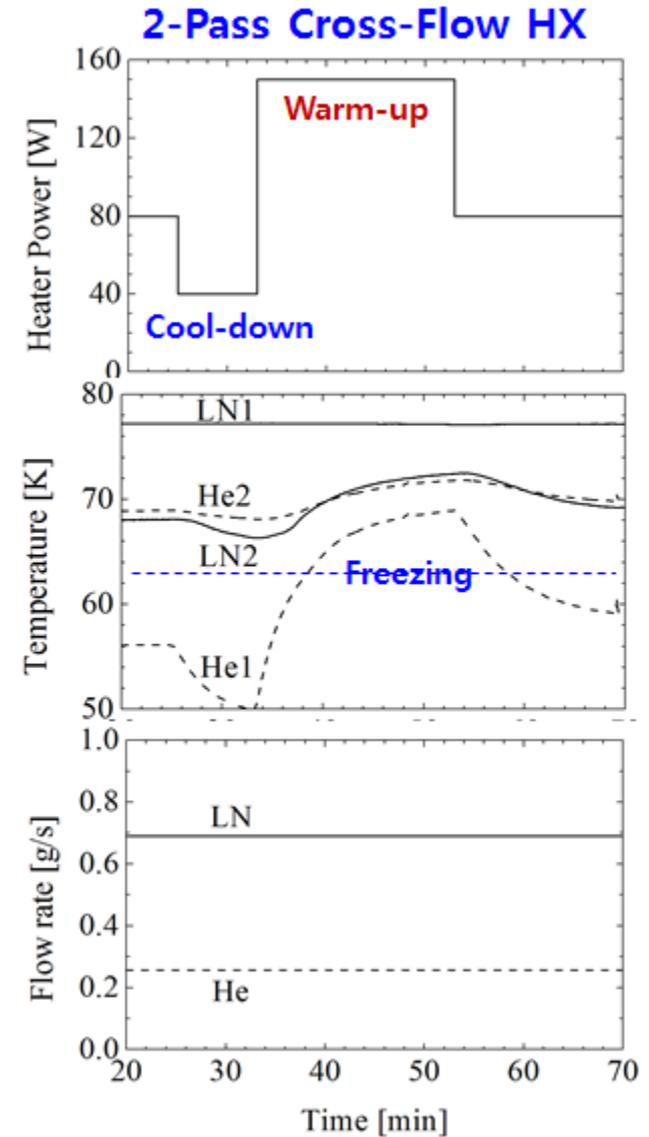


➤ Experimental Results (Chang et al., Cryogenics, 2013)

Heater Power



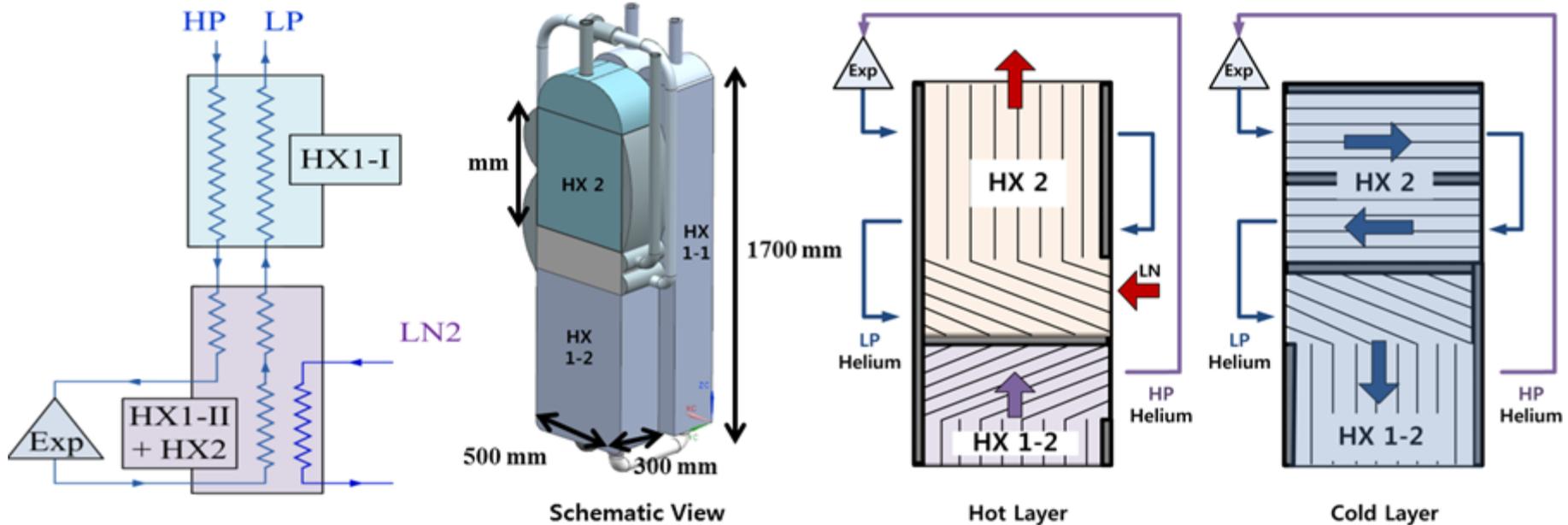
Temperature



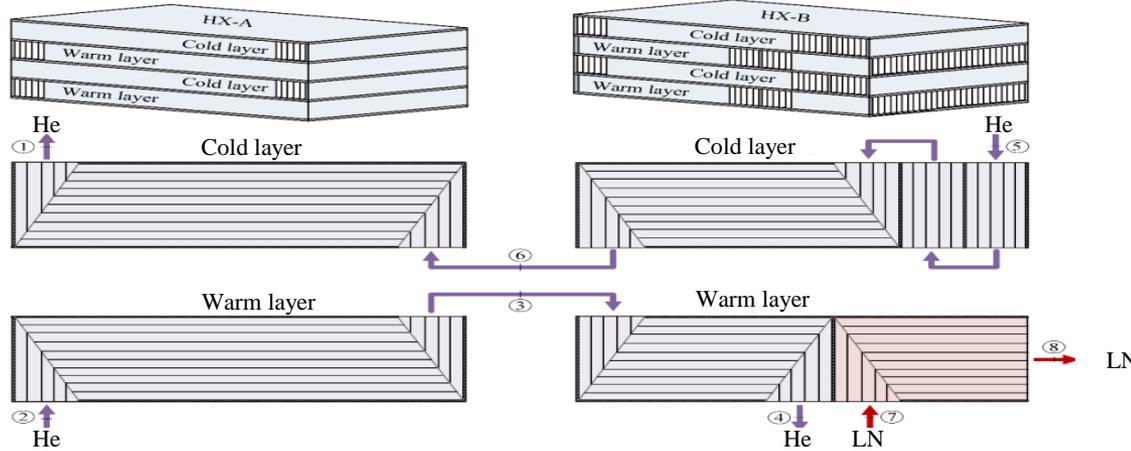
Flow Rate

## ➤ Application of 2-Pass Cross-Flow HX

- Based on the proven robustness to temporary freezing conditions
- Effective reduction of the freeze-out risk of LN<sub>2</sub>
- Compact design for He-He HX (10 kW Brayton refrigerator) and He-LN<sub>2</sub> HX



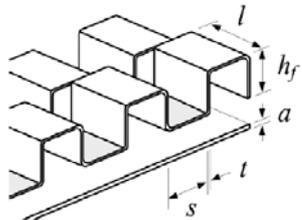
## ➤ Modified HX Design (Chang et al., Physics Procedia, 2015)



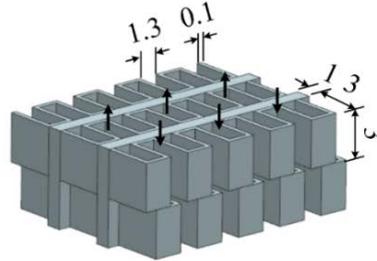
HX-A He + He 141 kW

HX-B He + He 66 kW

He + LN<sub>2</sub> 10 kW

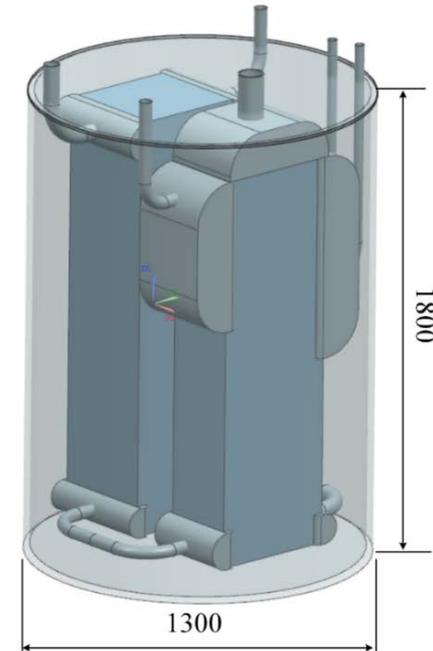
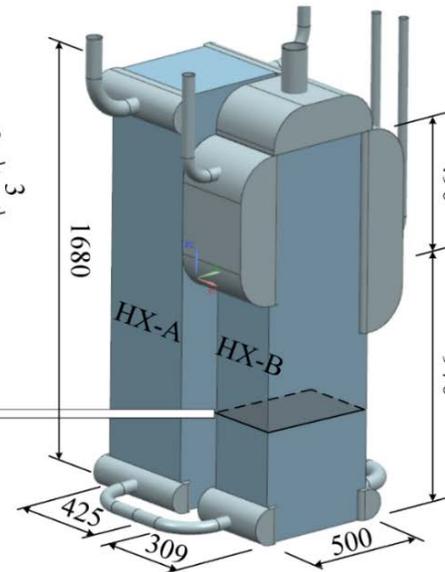
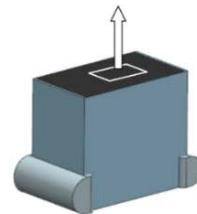


$$d = \frac{2h_f s}{h_f + s}$$

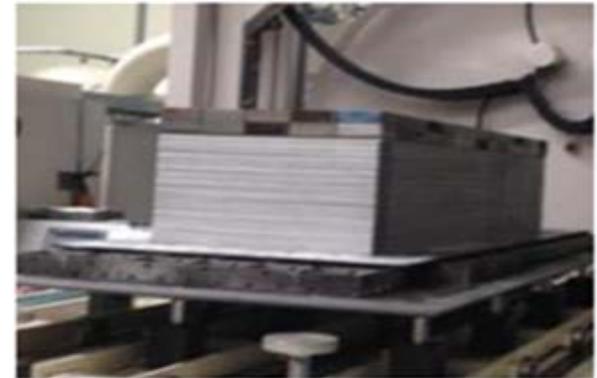


$$\eta = 1 - \frac{A_f}{A} \left[ 1 - \frac{\tanh(h_f \sqrt{h/2kt})}{h_f \sqrt{h/2kt}} \right]$$

$$\frac{1}{U_h} = \frac{1}{\eta_h h_h} + \frac{a A_h}{k A_w} + \frac{A_h}{\eta_c h_c A_c}$$



➤ Fabrication and Leak Test Completed (2015)

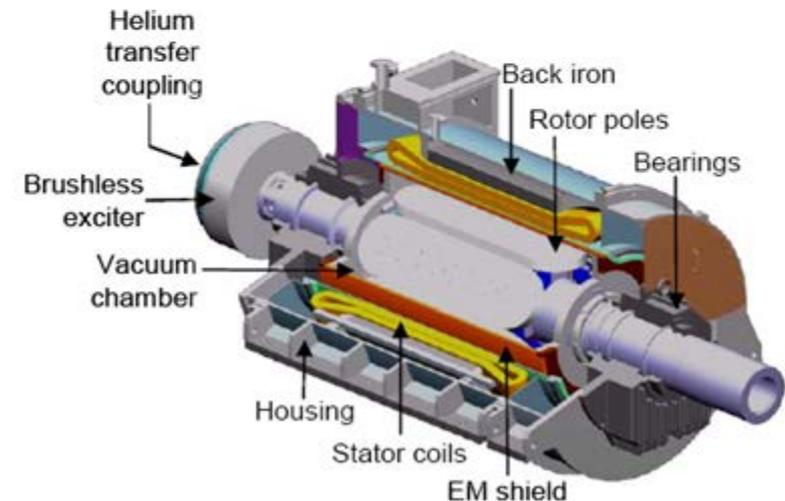
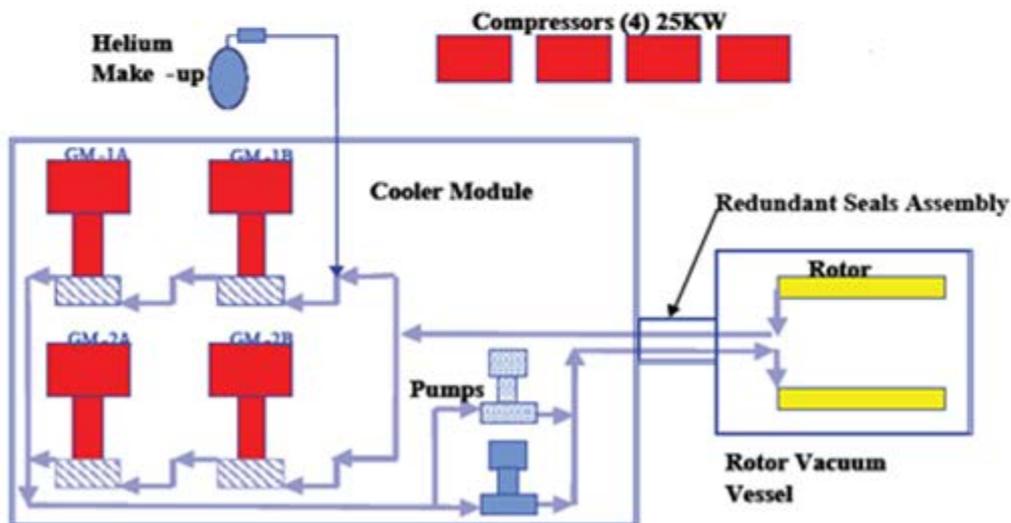
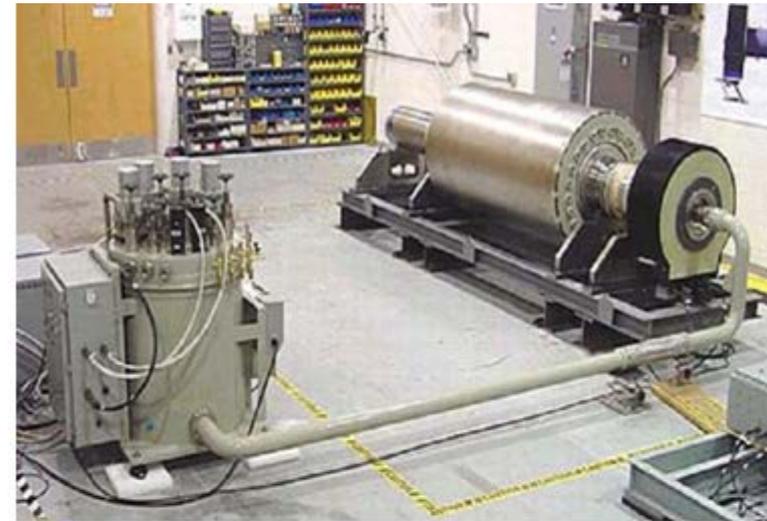


DongHwa Entec Co. (KOREA)

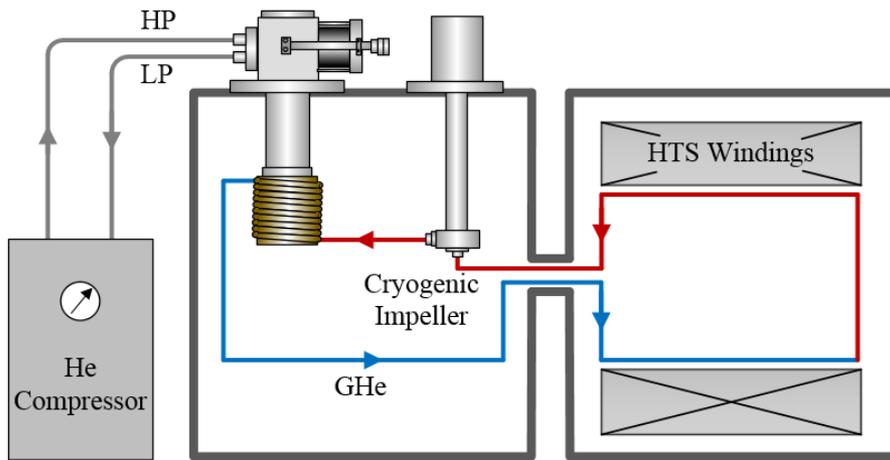
- Overview
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- He-LN<sub>2</sub> Heat Exchanger
- **Cryogenic Design for Future**

## ➤ Gas He Cooling System for HTS Motors

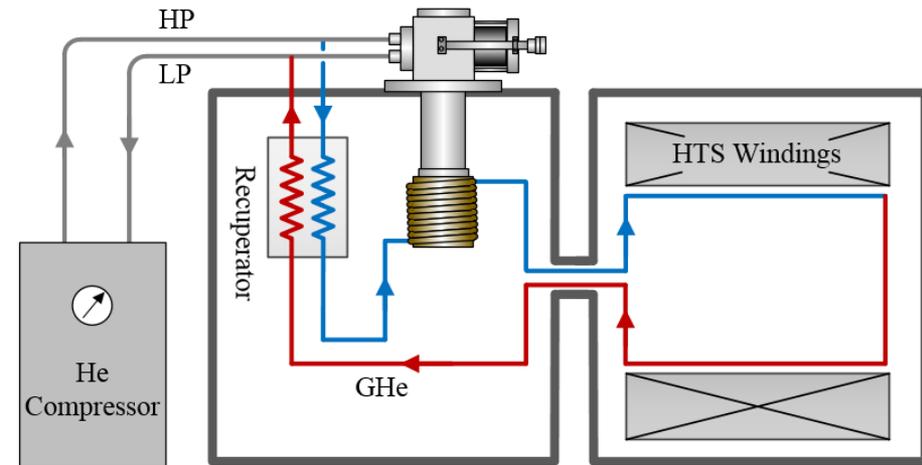
- U.S. Navy program
- Tested at CAPS (FL, USA, 2004)
- 5 MW shipboard motor and drive
- 4 units of **single-stage GM coolers** (AL330)
- **Gas He** circulation for cooling



Two **Separate** Cycles of GM Cooler and He Circulation



**Integrated** Cycle of GM Cooler and He Circulation



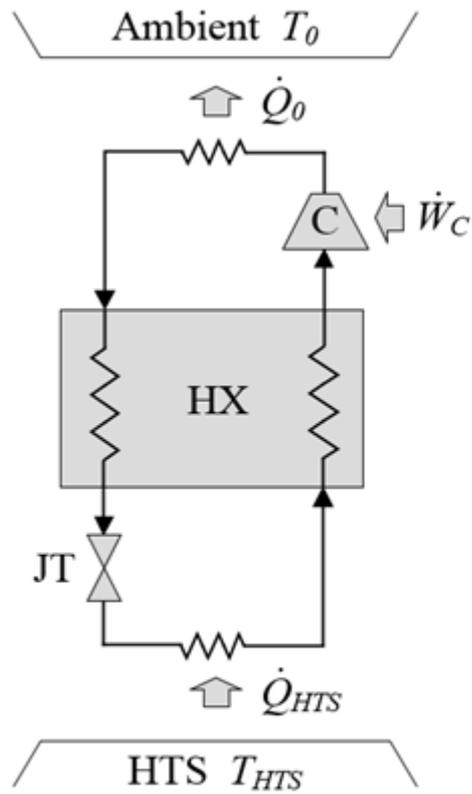
## ➤ Integrated Cycle

- **No cryogenic impeller or pump** is needed.
- Use of compressor unit for supplying **clean He gas** to the circulation loop
- **A larger capacity** of He compressor is needed
- **A recuperative HX** is needed for thermal regeneration
- Practical design by Cryomech (USA), Hyundai HI + Hong Ik University (KOREA)

Existing Design		Proposed (New) Design
Refrigeration	LN <sub>2</sub> Circulation	Integration of Refrigeration and LN <sub>2</sub> Circulation
Brayton Cycle Stirling Cycle	Pumped Circulation	(Claude Cycle?)
Gas He (Ne)	LN <sub>2</sub>	Gas N <sub>2</sub> + LN <sub>2</sub>
He Comp + He Exp	LN <sub>2</sub> Pump	N <sub>2</sub> Comp + N <sub>2</sub> Exp (No LN <sub>2</sub> Pump)
<p>Gas Refrigeration</p> <p>Use of (Limited) Commercial Coolers</p> <p>Small Power Input for Circulation</p>		<p>Proven Technology with N<sub>2</sub> Liquefaction</p> <p>Easy Scale-up for Longer Cables</p> <p>No Danger of LN<sub>2</sub> Freeze-out</p>

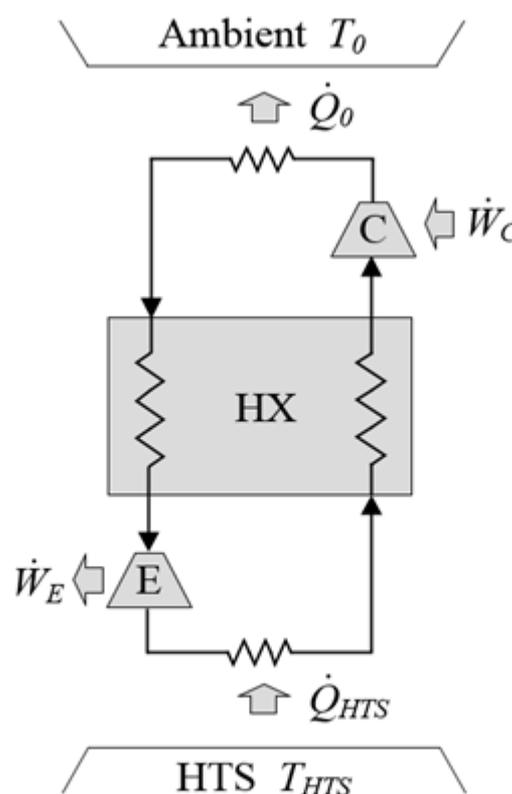
## ➤ Recuperative Refrigeration Cycles

### JT (Joule-Thomson) Cycle



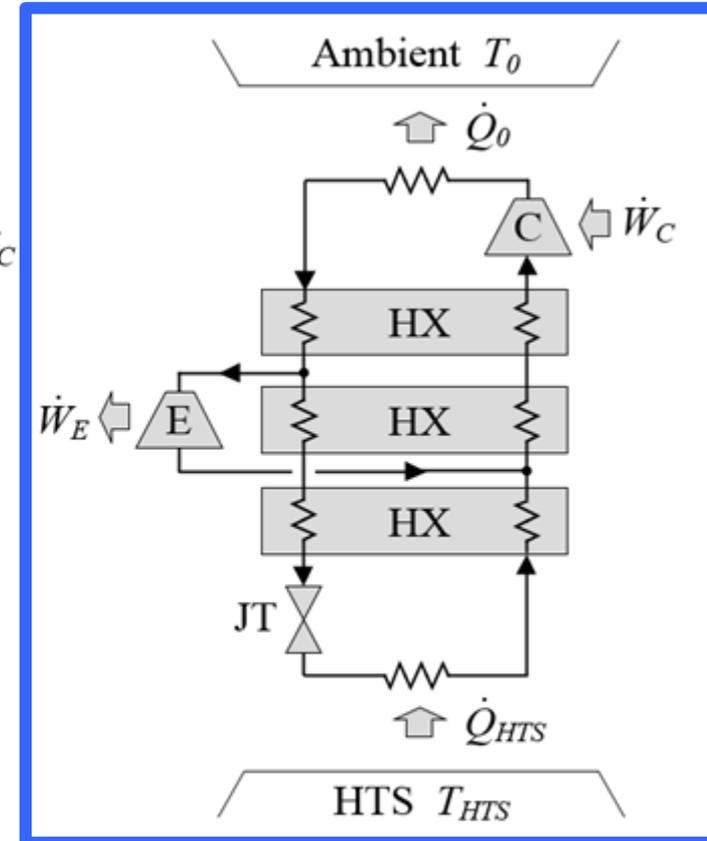
**JT Valve**  
**2-Phase Refrigerant**

### Brayton Cycle



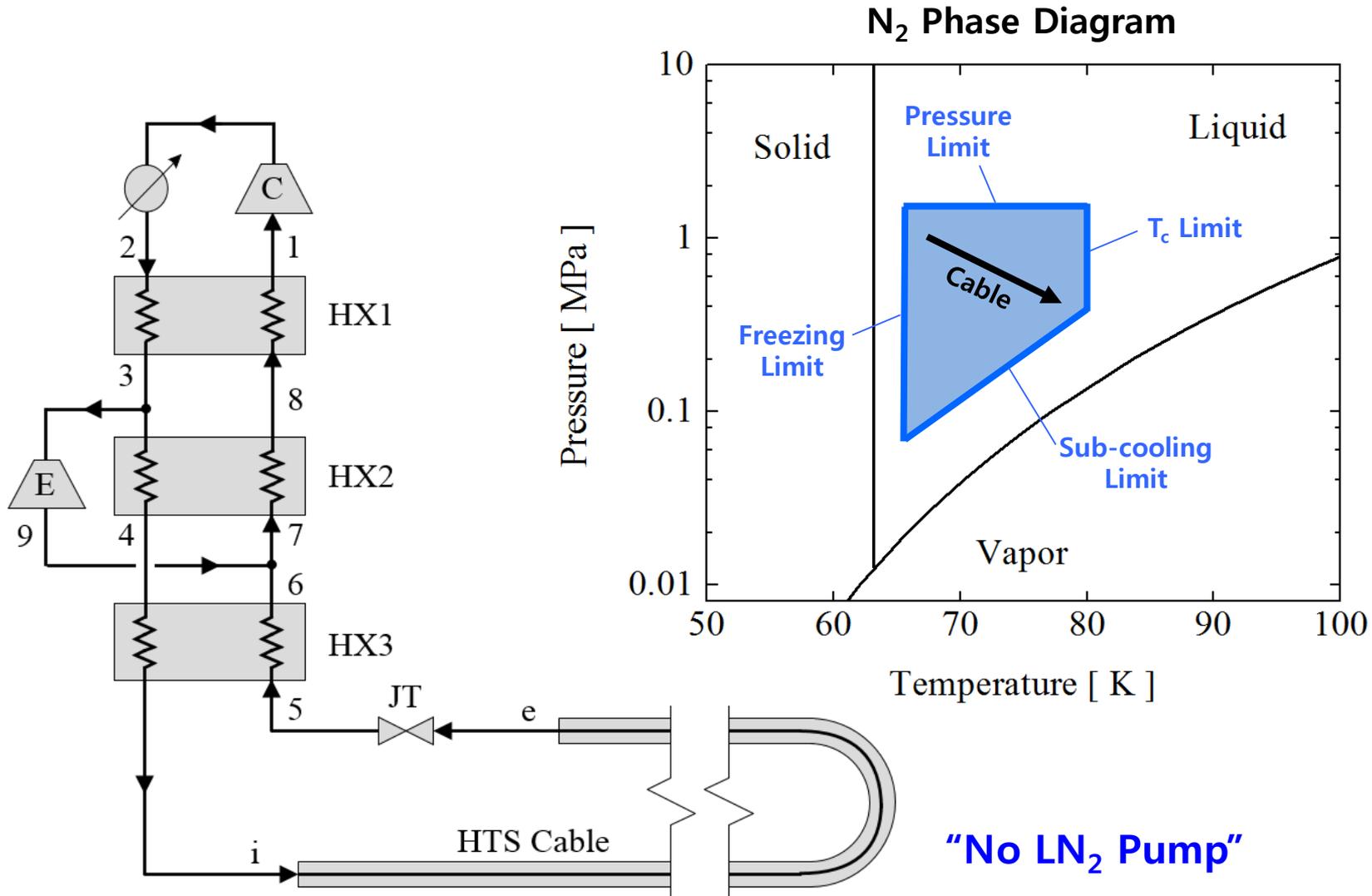
**Expander (Turbine)**  
**Gas Refrigerant**

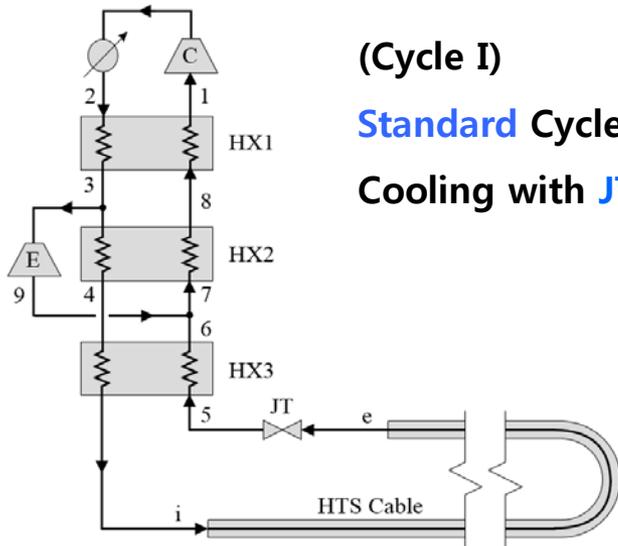
### Claude Cycle



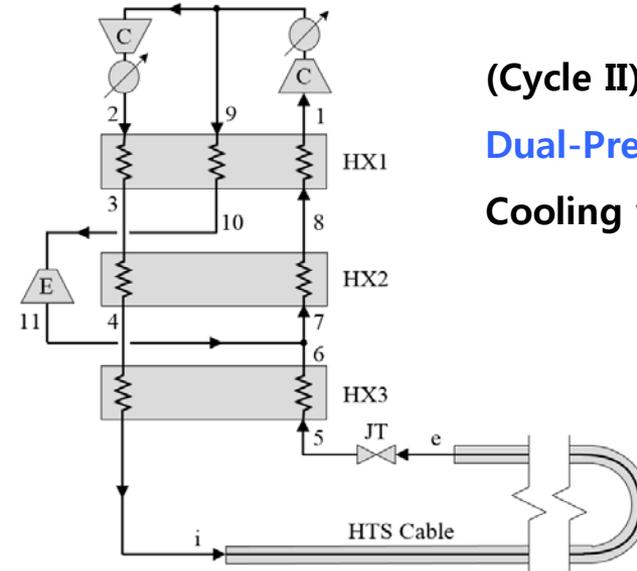
**JT Valve + Expander (Turbine)**  
**2-Phase Refrigerant**

## ➤ Cooling Requirements of HTS Cables and N<sub>2</sub> Claude Cycle

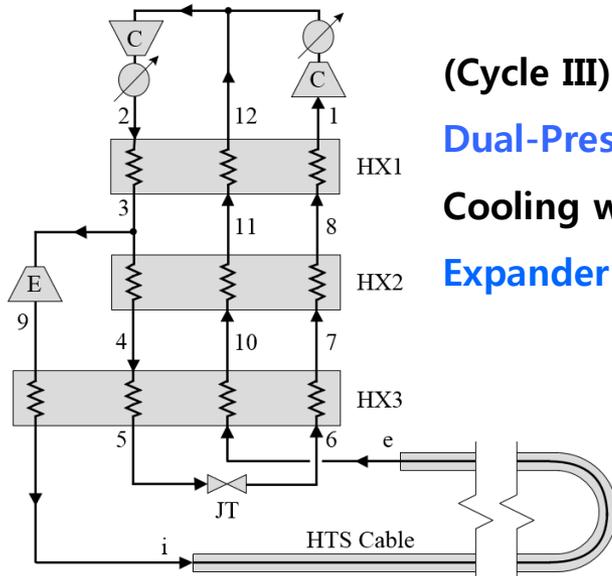




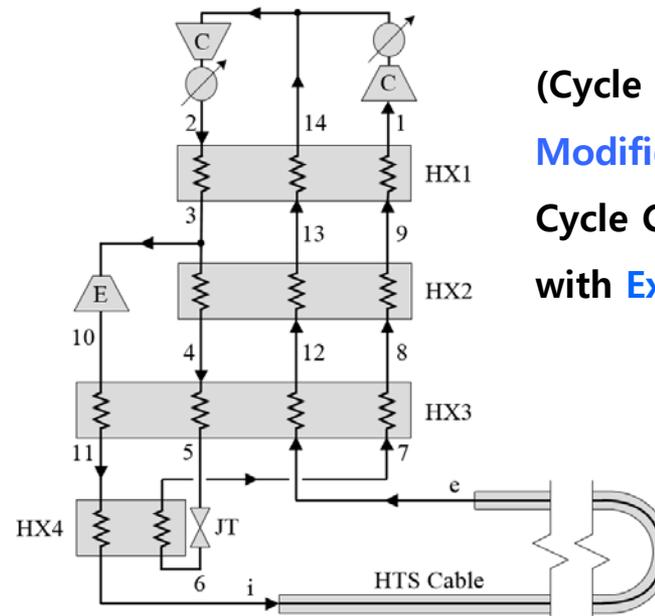
(Cycle I)  
Standard Cycle  
Cooling with JT Circuit



(Cycle II)  
Dual-Pressure Cycle  
Cooling with JT Circuit

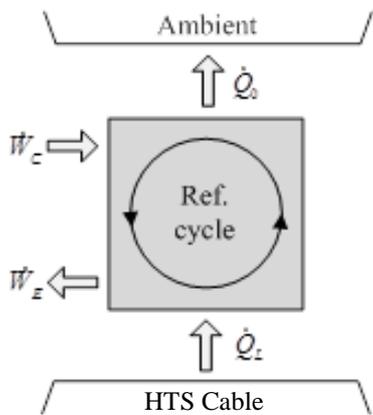


(Cycle III)  
Dual-Pressure Cycle  
Cooling with Expander Circuit



(Cycle IV)  
Modified Dual-Pressure Cycle Cooling  
with Expander Circuit

## ➤ Thermodynamics



(Energy)  $\dot{Q}_0 = (\dot{W}_C - \dot{W}_E) + \dot{Q}_{HTS}$

(Entropy)  $\frac{\dot{Q}_0}{T_0} = \frac{\dot{Q}_{HTS}}{T_{HTS}} + \dot{S}_{gen}$

FOM (Figure of Merit, %Carnot)

$$FOM = \frac{\dot{Q}_{HTS} \left( \frac{T_0}{T_{HTS}} - 1 \right)}{\dot{W}_C - \dot{W}_E}$$

Irreversibility

$$\begin{aligned} \dot{I} &= (\dot{W}_C - \dot{W}_E) - \dot{Q}_{HTS} \left( \frac{T_0}{T_{HTS}} - 1 \right) \\ &= T_0 \dot{S}_{gen} = T_0 \sum_i (\dot{S}_{gen})_i \end{aligned}$$

## ➤ Assumptions and Simulation Basis

- Ambient
- HTS Cable

Maximum T  
Thermal Load  
Supply and Return

$$T_0 = 300 \text{ K}$$

$$T_{HTS} = 78 \text{ K}$$

$$Q_{HTS} = 10 \text{ kW}$$

$$T_e - T_i = (78 \text{ K}) - (69 \text{ K}) = 9 \text{ K}$$

$$P_i - P_e = (0.65 \text{ MPa}) - (0.5 \text{ MPa}) = 0.15 \text{ MPa}$$

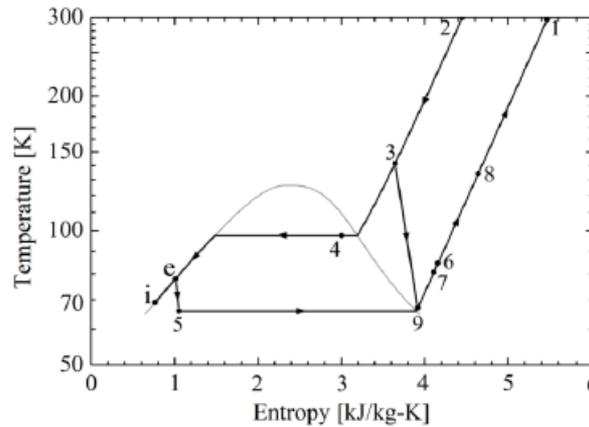
- Heat Exchangers

$$\Delta T_{min} = 3 \text{ K} \quad \Delta P = 0$$

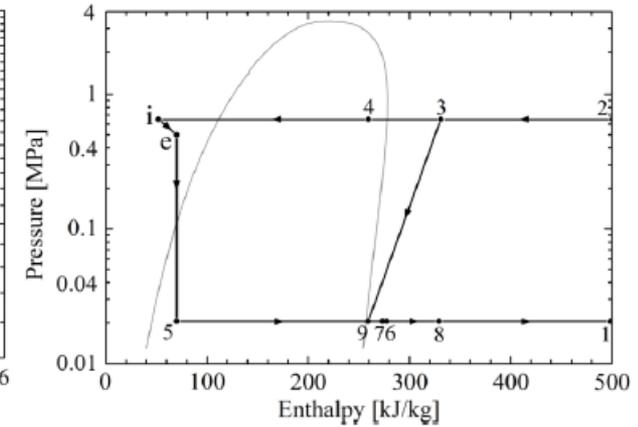
- Compressor & Expander

$$\eta_C = \eta_E = 80\%$$

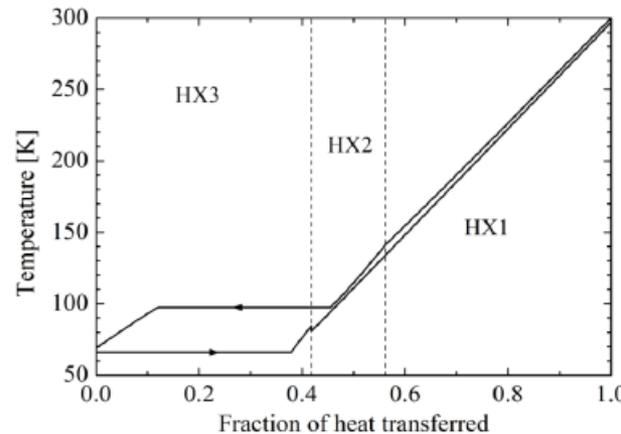
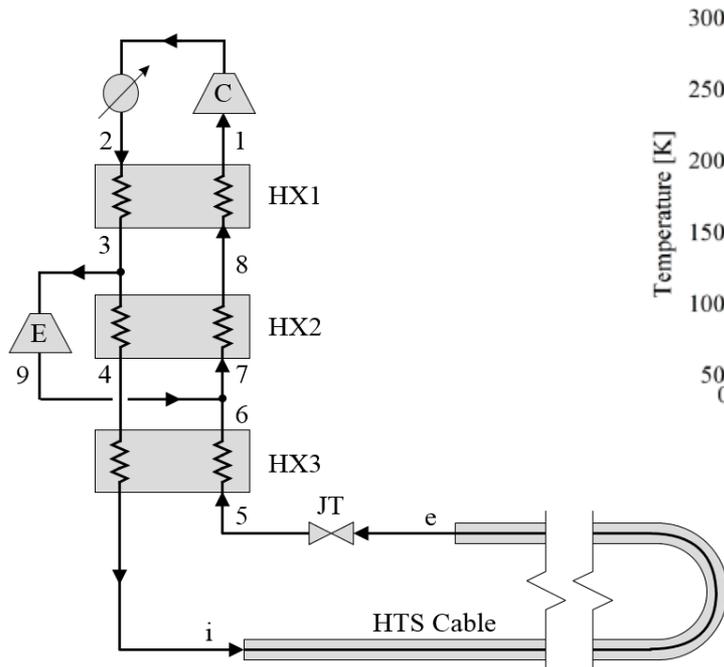
(Cycle I)  
Standard Cycle  
Cooling with  
JT Circuit



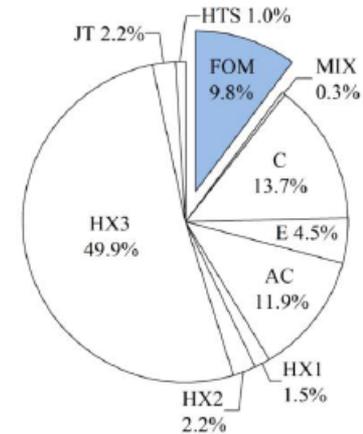
(a) T-s diagram



(b) P-h diagram

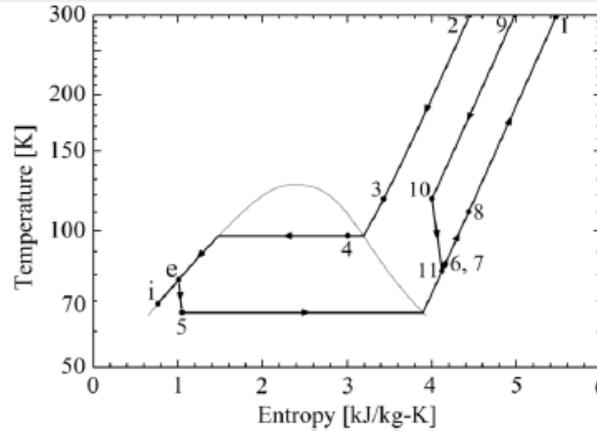


(c) Temperature profile in HX's

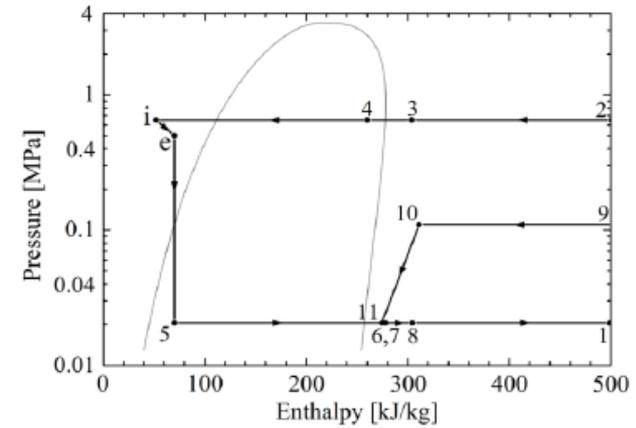


(d) Exergy expenditure

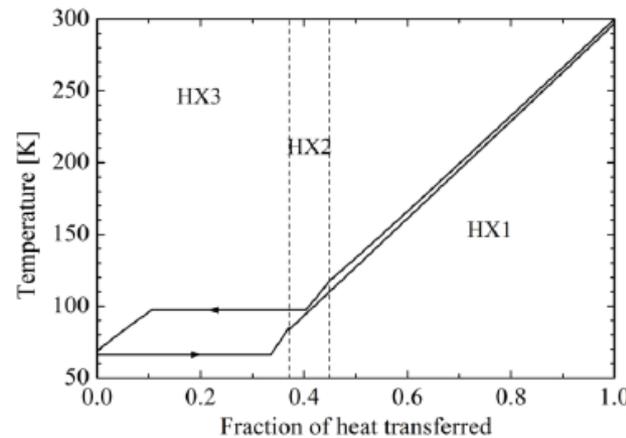
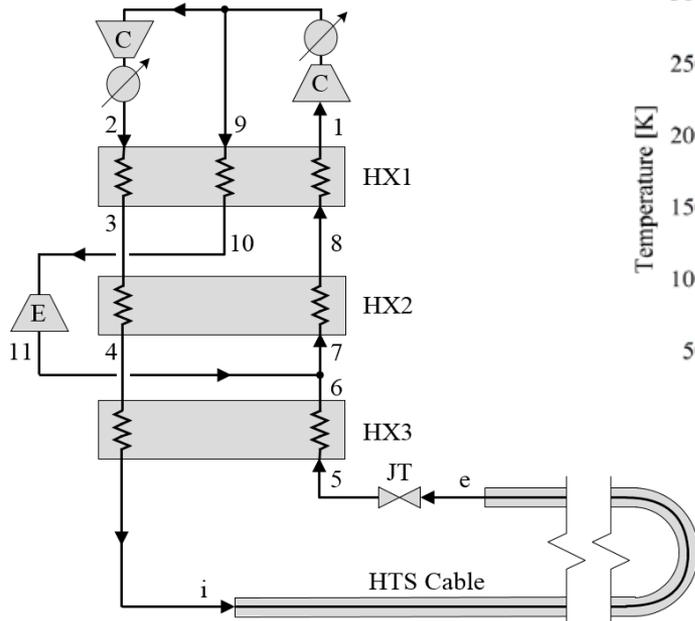
**(Cycle II)**  
**Dual-Pressure**  
**Cycle Cooling**  
**with JT Circuit**



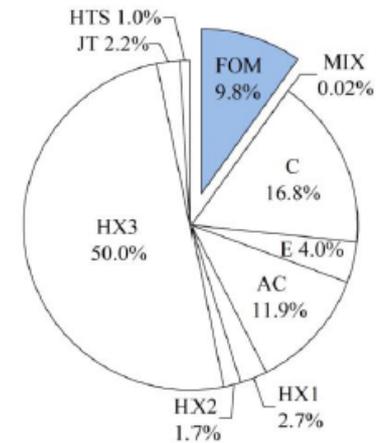
(a) T-s diagram



(b) P-h diagram

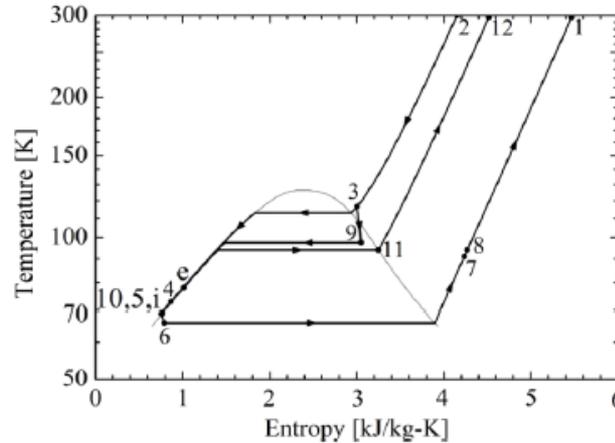


(c) Temperature profile in HX's

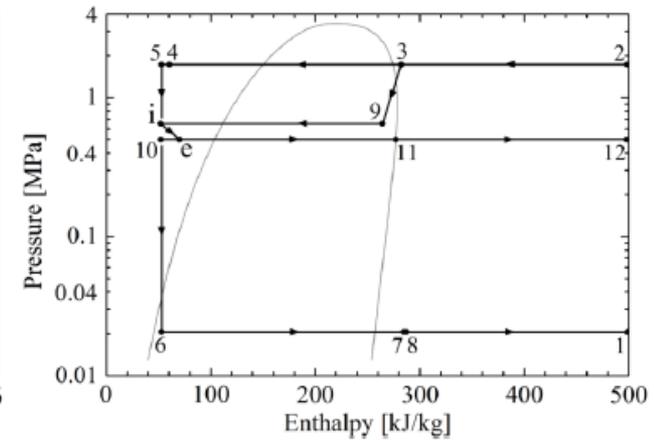


(d) Exergy expenditure

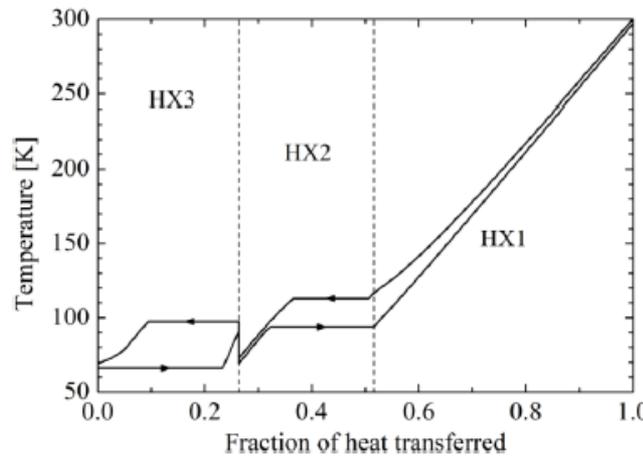
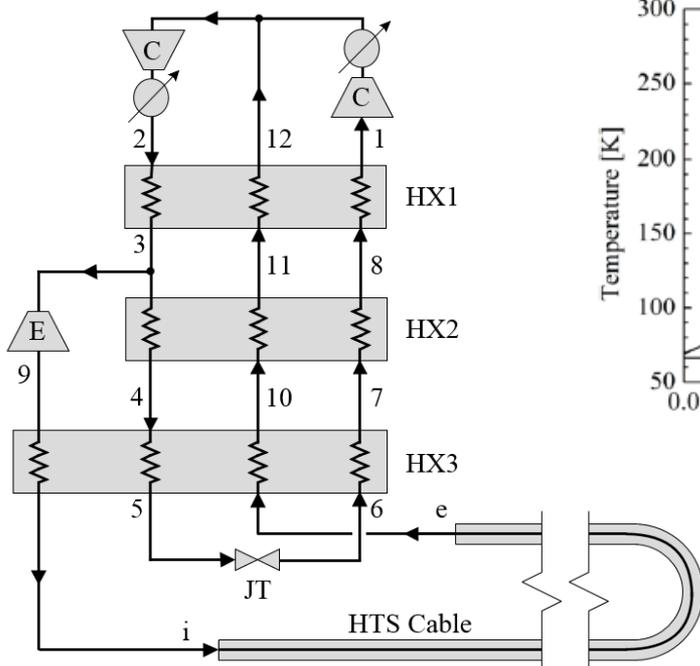
**(Cycle III)**  
**Dual-Pressure**  
**Cycle Cooling with**  
**Expander Circuit**



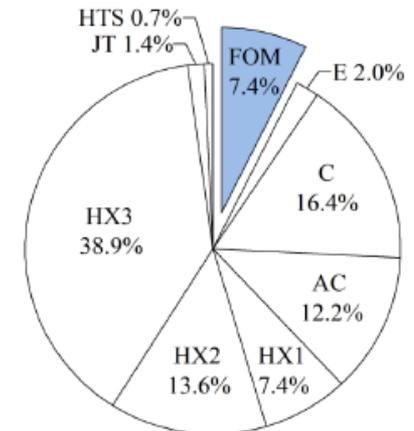
(a) T-s diagram



(b) P-h diagram

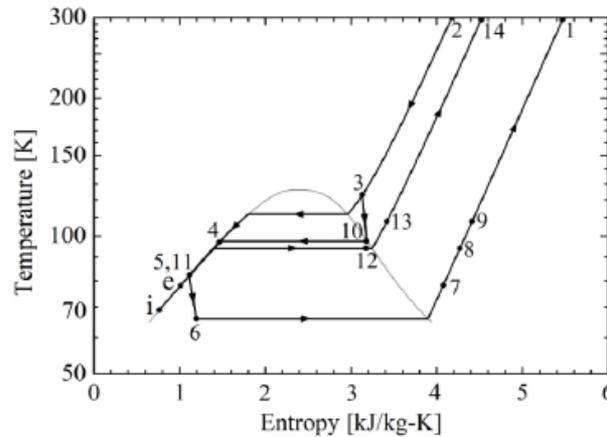


(c) Temperature profile in HX's

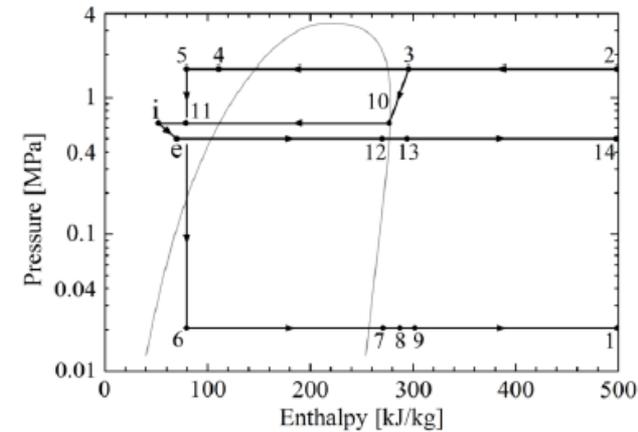


(d) Exergy expenditure

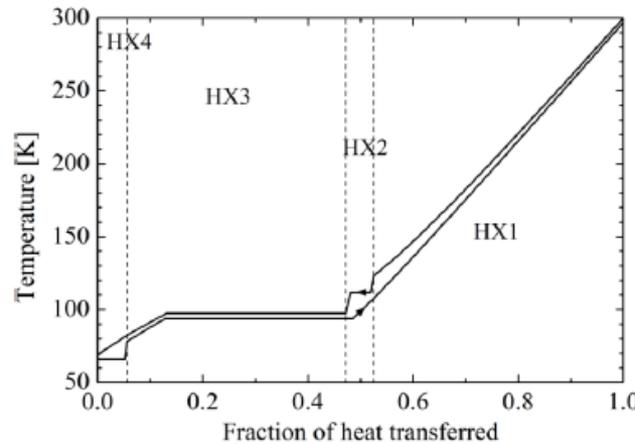
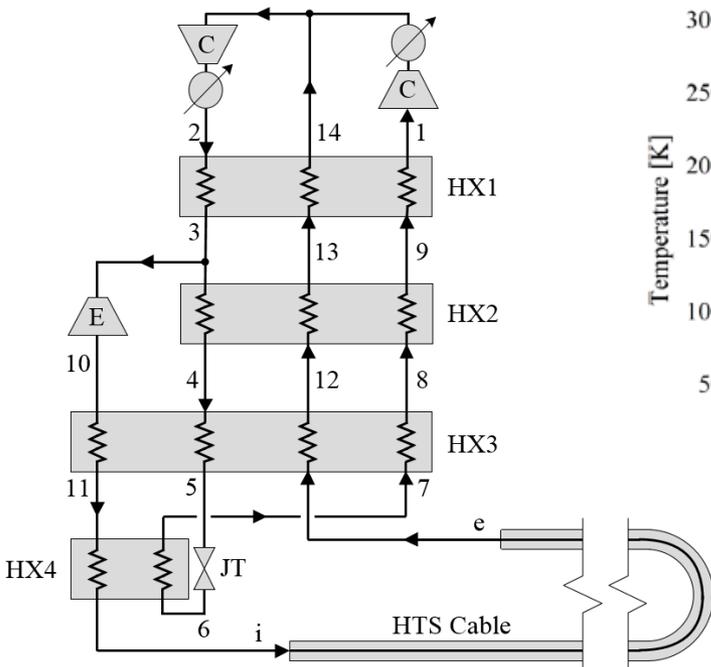
**(Cycle IV)**  
**Modified Dual-Pressure**  
**Cycle Cooling with**  
**Expander Circuit**



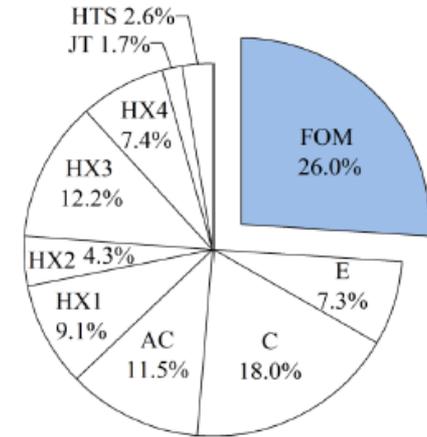
(a) T-s diagram



(b) P-h diagram



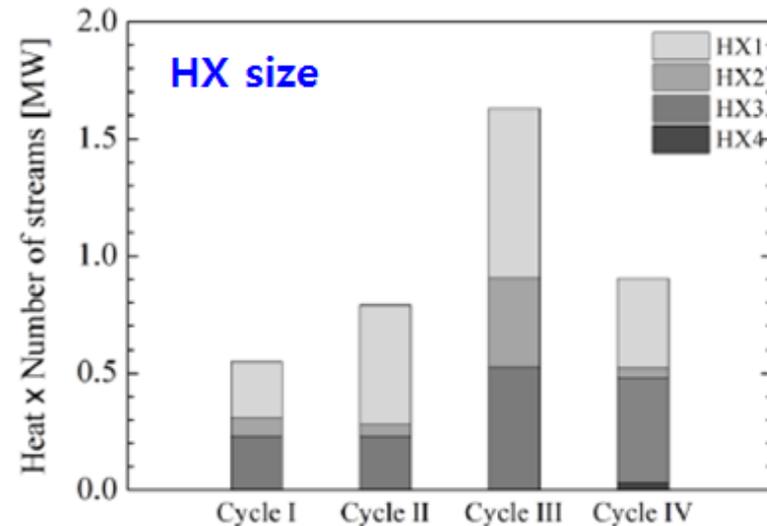
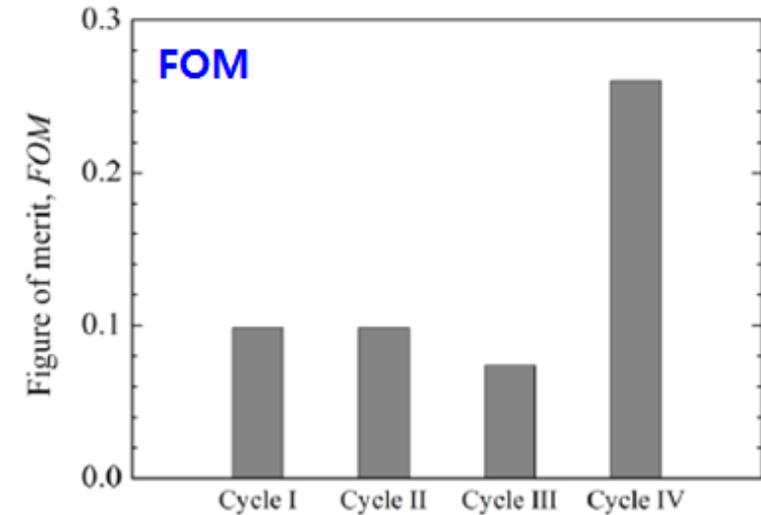
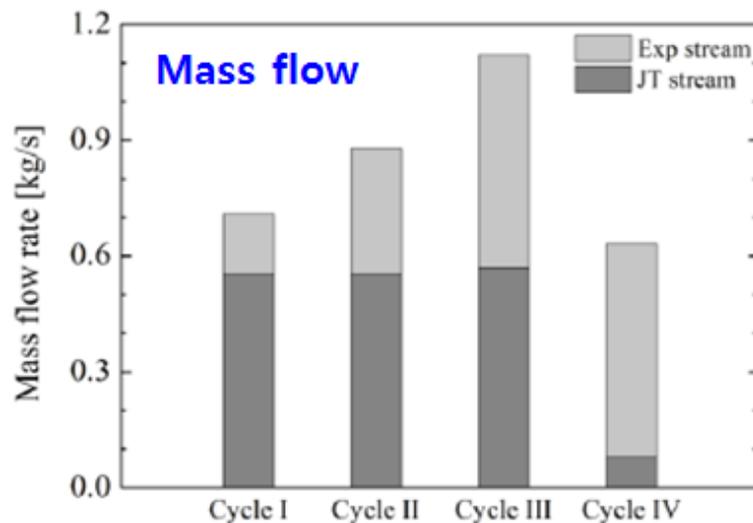
(c) Temperature profile in HX's



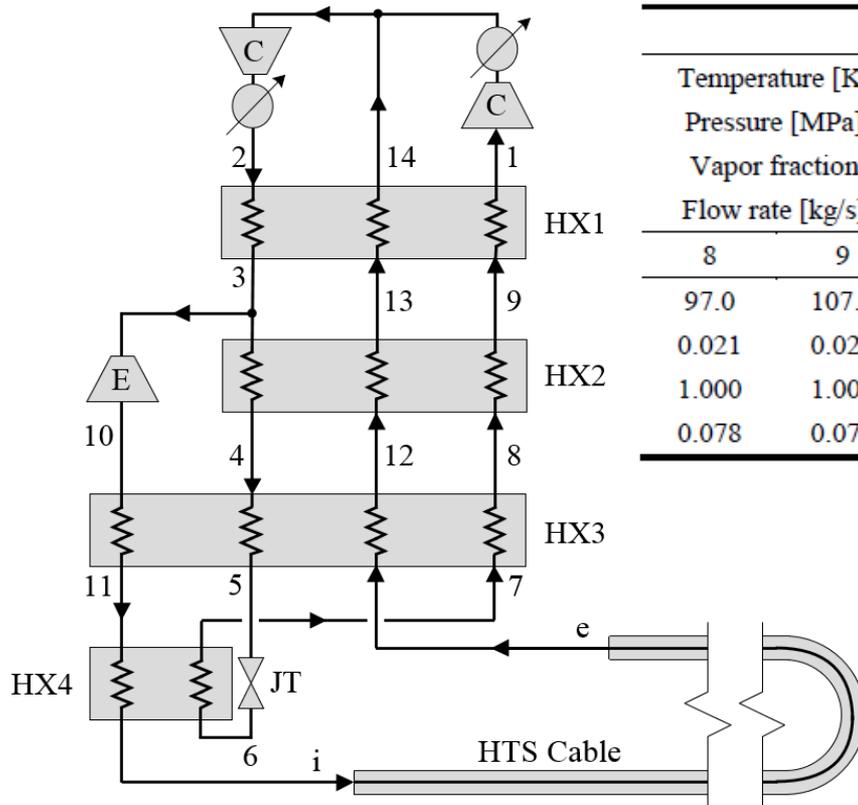
(d) Exergy expenditure

## ➤ Selection of Cycle

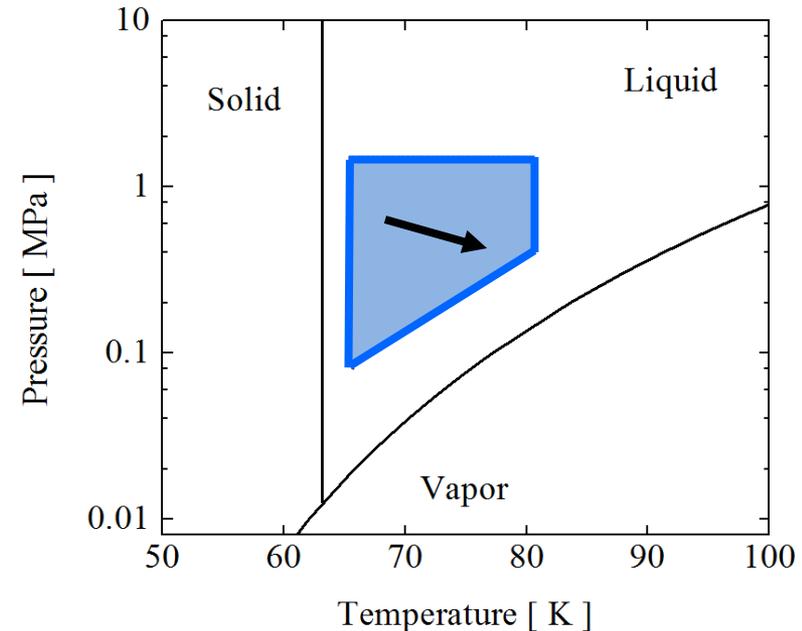
- Cycle (I) – **Simplest** and **Most Compact**
- Cycle (IV) – **Most Efficient** and **Smallest Comp** with Considerable improvement with **additional HX** due to reduced  $\Delta T$  in HX's



• Final Recommendation – **Cycle (IV)** Modified Dual-Pressure Claude Cycle



	1	2	3	4	5	6	7		
Temperature [K]	297.0	300.0	123.0	97.0	82.2	66.0	78.2		
Pressure [MPa]	0.021	1.610	1.610	1.610	1.610	0.021	0.021		
Vapor fraction	1.000	1.000	1.000	0.000	0.000	0.160	1.000		
Flow rate [kg/s]	0.078	0.631	0.631	0.078	0.078	0.078	0.078		
	8	9	10	11	i	e	12	13	14
Temperature [K]	97.0	107.6	97.5	82.2	69.0	78.0	94.0	107.6	297.0
Pressure [MPa]	0.021	0.021	0.650	0.650	0.650	0.500	0.500	0.500	0.500
Vapor fraction	1.000	1.000	1.000	0.000	0.000	0.000	0.961	1.000	1.000
Flow rate [kg/s]	0.078	0.078	0.553	0.553	0.553	0.553	0.553	0.553	0.553



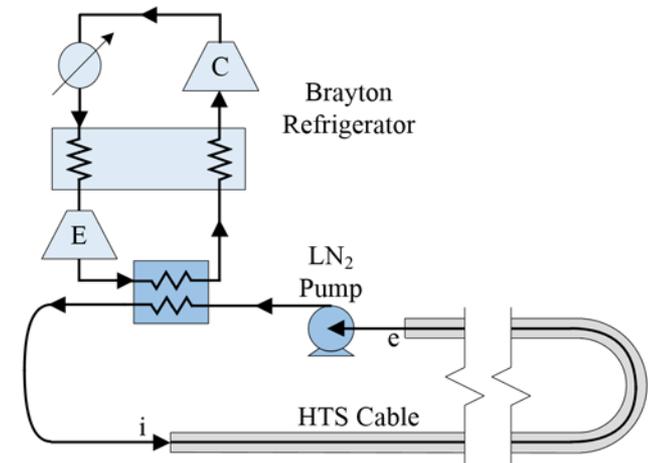
- Satisfaction of **cooling requirements**
- **Sub-atmospheric** operation
- Patent application underway

## ➤ HTS Cable Projects in Korea

- Great advantage of **high power density**
- A world record of **154 kV 1 km** Cable in Jeju

## ➤ 10 kW Brayton Refrigerator

- Viable option for 1 km Cables
- **Thermodynamic design** and construction with He (refrigerant)



## ➤ He-LN<sub>2</sub> Heat Exchanger

- 2-Pass **Cross-Flow HX** as anti-freezing scheme of LN<sub>2</sub>
- Detailed design and fabrication of plate-fin HX

## ➤ Cryogenic Design for future

- Integration of refrigerator and LN<sub>2</sub> circulation system
- Proposal of **modified Claude cycle** for long-length (1~3 km) cables